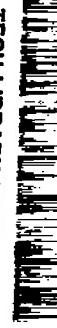




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RESEARCH MEMORANDUM

THEORETICAL ROCKET PERFORMANCE OF LIQUID METHANE WITH
SEVERAL FLUORINE-OXYGEN MIXTURES ASSUMING
FROZEN COMPOSITION

By Sanford Gordon and Michael E. Kastner

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THEORETICAL ROCKET PERFORMANCE OF LIQUID METHANE
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SUMMARY

Theoretical rocket performance for frozen composition during expansion was calculated for liquid methane with several fluorine-oxygen mixtures for a range of pressure ratios and oxidant-fuel ratios. The parameters included are specific impulse, combustion-chamber temperature, nozzle-exit temperature, molecular weight, characteristic velocity, coefficient of thrust, ratio of nozzle-exit area to throat area, specific heat at constant pressure, isentropic exponent, viscosity, and thermal conductivity.

The maximum calculated value of specific impulse for a chamber pressure of 600 pounds per square inch absolute (40.827 atm) and an exit pressure of 1 atmosphere is 315.3 for 79.67 percent fluorine in the oxidant.

INTRODUCTION

Mixtures of liquid fluorine and liquid oxygen as oxidants with hydrocarbons as fuel have been considered in recent years for possible high-energy rocket propellants. References 1 to 3 present data for JP-4 fuel with several mixtures of oxygen and fluorine. These data show that mixtures of fluorine and oxygen exist that give higher performance with JP-4 fuel than either 100 percent oxygen or fluorine because fluorine burns preferentially with hydrogen, and oxygen with carbon.

A hydrocarbon fuel with a higher hydrogen-carbon atom ratio than that of JP-4 fuel (1.942 hydrogen-carbon atom ratio) might be expected to yield even higher values of specific impulse with mixtures of fluorine and oxygen than were obtained with JP-4 fuel. Calculations were, therefore, made at the NACA Lewis laboratory in order to determine the performance of liquid methane with several mixtures of liquid fluorine and oxygen.

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SYMBOLS

The following symbols are used in this report:

- A nozzle area, sq in.
- a local velocity of sound, ft/sec
- C_F coefficient of thrust, $C_F = g_c I/c^* = F/P_c A_t$
- C_p^o molar specific heat at constant pressure, cal/(mole)(°K)
- c_p specific heat at constant pressure, $\frac{\sum_i x_i (C_p^o)_i}{M(1 - x_k)}$, cal/(g)(°K)
- c_v specific heat at constant volume
- c^* characteristic velocity, $g_c P_c A_t / w$, ft/sec
- F thrust, lb
- g_c gravitational conversion factor, 32.174 (lb mass/lb force)(ft/sec²)
- H_T^o sum of sensible enthalpy and chemical energy at temperature T, cal/mole
- h sum of sensible enthalpy and chemical energy per unit mass, $\frac{\sum_i x_i (H_T^o)_i}{M(1 - x_k)}$, cal/g
- I specific impulse, (lb force)(sec)/lb mass
- k coefficient of thermal conductivity, cal/(sec)(cm)(°K)
- M molecular weight, $\frac{\sum_i x_i M_i}{1 - x_k}$, g/g-mole or lb/lb-mole
- O/F oxidant-fuel weight ratio
- P static pressure (sum of partial pressures), lb/sq in.
- p partial pressure, lb/sq in.

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- R universal gas constant (consistent units)
 - r equivalence ratio, ratio of four times the number of carbon atoms plus the number of hydrogen atoms to two times the number of oxygen atoms plus the number of fluorine atoms, $\frac{4(C) + (H)}{2(O) + (F)}$
 - S_T^0 entropy at a pressure of 1 atmosphere, cal/(mole)(°K)

$$S_T^0 = \sum_i x_i (S_T^0)_i - \frac{R}{PM} \sum_j p_j \ln(p_j/14.696)$$
 - s entropy per unit mass, $\frac{\sum_i x_i (S_T^0)_i}{M(1 - x_k)} - \frac{R}{PM} \sum_j p_j \ln(p_j/14.696)$, cal/(g)(°K)
 - T temperature, °K
 - w mass-flow rate, lb/sec
 - x mole fraction
 - r isentropic exponent, $\left(\frac{\partial \ln P}{\partial \ln \rho}\right)_s$
 - ε ratio of nozzle area to throat area
 - μ absolute viscosity, g/(cm)(sec) or poises
 - ρ density, lb/cu in.

Subscripts:

- c combustion chamber
- e nozzle exit
- i product of combustion including both gaseous and solid phases
- j gaseous product of combustion
- k solid product of combustion (graphite)
- p constant pressure
- s constant entropy

t nozzle throat

Superscript:

- o thermodynamic standard reference state

CALCULATION OF PERFORMANCE DATA

Performance data were obtained for liquid methane with several fluorine-oxygen mixtures for a range of equivalence and pressure ratios. Frozen composition during expansion from a chamber pressure of 600 pounds per square inch absolute was assumed.

The computations were carried out by the method described in reference 4 with modifications to adapt it for use with an IBM card-programmed electronic calculator. The machine was operated with floating-decimal-point notation and eight significant figures. The successive approximation process used in the calculations was continued until seven-figure accuracy was reached in the desired values of the assigned parameters (mass balance and pressure or entropy).

Assumptions

The calculations were based on the following usual assumptions: perfect gas law, adiabatic combustion at constant pressure, isentropic expansion, no friction, homogeneous mixing, and one-dimensional flow. The products of combustion were assumed to be graphite and the following ideal gases: atomic carbon C, carbon monofluoride CF, carbon difluoride CF_2 , carbon trifluoride CF_3 , carbon tetrafluoride CF_4 , difluorocetylene C_2F_2 , methane CH_4 , carbon monoxide CO, carbon dioxide CO_2 , atomic fluorine F, fluorine F_2 , atomic hydrogen H, hydrogen H_2 , hydrogen fluoride HF, water H_2O , atomic oxygen O, oxygen O_2 , and the hydroxyl radical OH. The combustion products are assumed to be completely expanded within the exit nozzle; that is, ambient pressure equals exit pressure.

The graphite was assumed to be finely divided and in temperature and velocity equilibrium with the gases during the flow process.

Initial Data

Thermodynamic data. - The thermodynamic data for all combustion products except graphite, methane, the fluorocarbons, and water were taken from reference 4. Data for graphite were taken from reference 5, for carbon monofluoride from reference 6, for the remainder of the

fluorocarbons from reference 7, and for water from reference 8. Data for methane were determined by the rigid-rotator - harmonic-oscillator approximation using spectroscopic data from reference 9. The base used in this report for assigning absolute values to enthalpy is the same as in reference 4.

The dissociation energy of fluorine was assumed to be 35.6 kilocalories per mole and the heat of sublimation of graphite at 298.16° K was assumed to be 171.698 kilocalories per mole (ref. 10). The heat of solution of oxygen and fluorine was omitted.

Physical, thermochemical, and viscosity data. - Several properties of the propellants taken from references 4, 10, 11, and 12 are listed in table I. The viscosity data for the individual combustion products were either taken from the literature when available, or estimated. The viscosities of F, H, H₂, and HF are given in reference 13. The viscosities of the remaining substances except H₂O were calculated using similar techniques. The viscosity of H₂O was obtained from a modified Sutherland equation (ref. 14).

Formulas

Interpolation formulas and accuracy of results are discussed in reference 15. The formulas used in computing the various performance parameters are as follows:

Specific impulse, (lb force)(sec)/lb mass

$$I = 294.98 \sqrt{\frac{h_c - h_e}{1000}} \quad (1)$$

Throat area per unit mass-flow rate, (sq in.)(sec)/lb

$$\frac{A_t}{w} = \frac{2781.6 T_t}{P_t M_t a} \quad (2)$$

This equation is derived from the continuity equation and the fact that the velocity of flow equals the velocity of sound at the throat.

Characteristic velocity, ft/sec

$$c^* = g_c P_c \frac{A_t}{w} = 32.174 P_c \frac{A_t}{w} \quad (3)$$

Coefficient of thrust

$$C_F = \frac{gc^I}{c^*} = \frac{32.174 I}{c^*} \quad (4)$$

Nozzle area per unit mass-flow rate, (sq in.)(sec)/lb

$$\frac{A}{w} = \frac{86.455 T}{PM} \quad (5)$$

Ratio of nozzle area to throat area

$$\epsilon = \frac{A/w}{A_t/w} \quad (6)$$

Specific heat at constant pressure, cal/(g)(°K)

$$c_p = \frac{\sum x_i (c_p^0)_i}{M(1 - x_k)} \quad (7)$$

Isentropic exponent

$$\gamma = \left(\frac{\partial \ln P}{\partial \ln \rho} \right)_s \quad (8)$$

When the composition is frozen,

$$\left(\frac{\partial \ln P}{\partial \ln \rho} \right)_s = \frac{c_p}{c_p - \frac{R}{M}} = \frac{c_p}{c_v}$$

Absolute viscosity, poises

$$\mu = \frac{PM}{\sum_j \frac{p_j}{\mu_j/M_j}} \quad (9)$$

Coefficient of thermal conductivity, cal/(sec)(cm)(°K)

$$k = \mu \left(c_p + \frac{5}{4} \frac{R}{M} \right) \quad (10)$$

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THEORETICAL PERFORMANCE DATA

Tables

The calculated values of the various performance parameters for a combustion pressure of 600 pounds per square inch absolute and for a range of oxidant-fuel ratios and exit conditions are given in tables II to V for a range of fluorine-oxygen ratios.

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The fluorine-oxygen atom ratios selected are 0(100 percent oxygen), 0.2, 0.5, 1.0, 2.0, 3.0, 3.3, 3.4, 3.7, and 4.0, which correspond to the following percentages of fluorine in the oxidant by weight: 0, 19.19, 37.25, 54.29, 70.37, 78.08, 79.67, 80.15, 81.46, and 82.61. The range of oxidant-fuel ratios selected for each percentage of fluorine is greater for the fluorine percentages up to 70 than for those over 70. For the fluorine percentages over 70, closely spaced oxidant-fuel ratios were selected primarily to determine maximum specific impulse.

The properties of gases in the combustion chamber and the characteristic velocity are given in table II. Table III presents the values of the performance parameters at assigned temperatures and constant entropy. These values were computed directly and used to interpolate properties at the assigned pressure ratios given in table IV. Properties at the throat in table IV may be found where the ratio of nozzle area to throat area ϵ is 1.000. The values adjacent to the throat correspond to pressures of 1.2 and 0.8 times the throat pressure. Table V presents the equilibrium composition in the combustion chamber. Solid graphite did not appear as a combustion product for any of the conditions considered in this report and is therefore omitted from table V. The mole fractions of carbon tetrafluoride and methane were always less than 5×10^{-6} for all the conditions considered in this report and therefore these substances were also omitted from table V. Performance data for expansion from combustion-chamber pressure to 1 atmosphere are summarized in table VI.

Curves

The performance parameters are plotted in figures 1 to 7. Curves of specific impulse are presented in figure 1 for assigned pressure ratios as functions of percentages of fuel by weight.

Combustion temperature and exit temperature for assigned pressure ratios are plotted in figure 2 as functions of percentages of fuel by weight.

In figure 2(f) the combustion temperatures for 78.08, 79.67, 80.15, 81.46, and 82.61 percent fluorine in the oxidant by weight are presented as separate curves. However, the exit curves coincided so closely that only one curve is given for each pressure ratio covering the range of 78.08 to 82.61 percent fluorine.

Curves of the ratio of nozzle area to throat area are plotted in figure 3 as functions of percentages of fuel by weight for assigned pressure ratios.

Figures 4 and 5 present curves of molecular weight and characteristic velocity, respectively, as functions of percentages of fuel by weight.

Effect of fluorine-oxygen ratio. - The specific-impulse data for expansion from chamber pressure to 1 atmosphere (table VI) are plotted in figure 6 to show the effect of fluorine-oxygen ratios on performance. Specific impulse increases with increasing percentages of fluorine to about 80 percent fluorine in the oxidant. Increasing the amount of fluorine in the oxidant above 80 percent results in a decrease in specific impulse.

Maximum values of specific impulse calculated for a chamber pressure of 600 pounds per square inch absolute (40.827 atm) and an exit pressure of 1 atmosphere are shown in the following table:

Fluorine in oxidant, percent by weight	Maximum specific impulse, lb-sec / lb
0	282.8
19.19	289.0
37.25	295.3
54.29	301.8
70.37	310.0
78.08	315.1
79.67	315.3
80.15	315.2
81.46	314.2
82.61	312.7

The data of the preceding table are plotted in figure 7; it may be seen from this figure that a specific impulse value of about 315 may be obtained from about 77 to 81 percent fluorine in the oxidant. Specific impulse increases from 282.8 to 315.3 for 0 to 79.67 percent fluorine in the oxidant and decreases from 315.3 to 312.7 for 79.67 to 82.61 percent fluorine in the oxidant. A curve for JP-4 fuel with mixtures of fluorine

and oxygen (fig. 8 of ref. 2) is also given in figure 7 for comparison. The maximum value of specific impulse for JP-4 fuel is 301.6 at about 70 percent fluorine in the oxidant as compared with 315.3 at 79.67 percent fluorine in the oxidant for liquid methane.

Effect of finite chamber area. - The use of a combustion chamber of finite cross-sectional area leads to a pressure change across the combustion process. Reference 15 illustrates how the data for low pressure ratios may be used to calculate the pressure at the injector face.

SUMMARY OF RESULTS

A theoretical investigation of the performance of liquid methane with fluorine-oxygen mixtures was made for the following conditions: fluorine in oxidant by weight from 0 to 82.61 percent for various equivalence ratios, pressure ratios from 1 to 300, and frozen composition during expansion from 600 pounds per square inch absolute in the combustion chamber. The maximum values of specific impulse calculated for an exit pressure of 1 atmosphere (pressure ratio, 40.827) ranged from 282.8 to 315.3 for 0 to 79.67 percent fluorine in the oxidant and from 315.3 to 312.7 for 79.67 to 82.61 percent fluorine in the oxidant.

Lewis Flight Propulsion Laboratory
National Advisory Committee for Aeronautics
Cleveland, Ohio, February 27, 1958

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TABLE I. - PROPERTIES OF LIQUID PROPELLANTS

Property	Propellant		
	Oxygen, O ₂	Fluorine, F ₂	Methane, CH ₄
Molecular weight, M	32.00	38.00	16.042
Density, g/cc	^a 1.1415	^b 1.54	^c 0.4245
Freezing point, °C	^{d,e} -218.76	^d -217.96	^{d,f} -182.48
Boiling point, °C	^d -182.97	^d -187.92	^d -161.49
Enthalpy of formation at boiling point from ele- ments at 25° C, kcal/mole	^g -3.080	^g -3.030	^{d,h} -21.352
Enthalpy of vaporization, kcal/mole	^{d,i} 1.630	^{d,j} 1.51	^{d,k} 1.955
Enthalpy of fusion, kcal/mole	^{d,l} 0.106	^{d,m} 0.372	^{d,n} 0.225

^aAt -182.0° C; ref. 11.^bAt -196° C; ref. 12.^cAt -161.5° C; ref. 11.^dRef. 10.^eAt 1.1 mm Hg.^fAt 87.7 mm Hg.^gRef. 4.^hUnpublished NACA calcula-
tions based on data of
ref. 9.ⁱAt -182.97° C.^jAt -187.92° C.^kAt -161.49° C.^lAt -218.76° C.^mAt -217.96° C.ⁿAt -182.48° C.

TABLE II. - THERMODYNAMIC PROPERTIES OF COMBUSTION-CHAMBER GASES AND CHARACTERISTIC
VELOCITY FOR LIQUID METHANE WITH SEVERAL MIXTURES OF FLUORINE AND OXYGEN

Equiv-a-lence ratio, $r = \frac{4(C) + (H)}{2(O) + (F)}$	Fuel, percent by weight	Oxidant-to-fuel weight ratio, O/F	Temper-ature, T, °K	Molecular weight, M	Enthalpy, h, cal/g (a)	Entropy, s, cal/(g)°K (b)	Specific heat, c, cal/(g)°K (b)	Iso-entropic exponent, γ (b)	Charac-teristic velocity, c*, ft/sec (b)
Percent fluorine in oxidant, 0 (100 percent oxygen)									
1.00	20.04	3.990	3497	22.87	2645.8	2.8259	0.519	1.201	5700
1.30	24.58	3.069	3444	20.54	3237.1	3.0420	.565	1.207	5959
1.40	25.98	2.850	3372	19.80	3419.6	3.1038	.578	1.210	5998
1.50	27.32	2.660	3272	19.08	3595.5	3.1804	.590	1.215	6011
1.60	28.62	2.493	3147	18.39	3765.0	3.2121	.600	1.220	5996
1.80	31.09	2.216	2855	17.10	4086.6	3.3011	.618	1.231	5901
Percent fluorine in oxidant by weight, 19.19									
1.20	21.10	3.740	3622	20.83	3017.6	2.9809	0.521	1.224	6036
1.40	23.78	3.206	3536	19.59	3359.2	3.1015	.548	1.227	6145
1.50	25.05	2.992	3460	18.99	3521.4	3.1556	.560	1.230	6169
1.60	26.28	2.805	3362	18.40	3678.2	3.2056	.571	1.233	6172
1.80	28.62	2.493	3119	17.28	3977.0	3.2936	.591	1.242	6118
Percent fluorine in oxidant by weight, 37.25									
1.30	20.35	3.913	3753	19.88	3145.8	3.0158	0.505	1.247	6248
1.50	22.77	3.391	3650	18.86	3447.2	3.1221	.530	1.248	6324
1.60	23.83	3.179	3572	18.36	3591.2	3.1701	.541	1.250	6336
1.70	25.05	2.992	3479	17.87	3730.9	3.2147	.552	1.252	6333
1.90	27.19	2.677	3258	16.95	3998.3	3.2945	.571	1.258	6282
Percent fluorine in oxidant by weight, 54.29									
1.30	18.26	4.475	3957	19.60	3100.6	2.9706	0.476	1.271	6416
1.40	19.40	4.158	3917	19.16	3238.7	3.0222	.488	1.270	6459
1.50	20.50	3.879	3864	18.73	3375.1	3.0708	.499	1.270	6489
1.60	21.57	3.636	3798	18.30	3503.9	3.1165	.511	1.270	6506
1.80	23.63	3.232	3628	17.48	3755.1	3.1994	.531	1.272	6503
Percent fluorine in oxidant by weight, 70.37									
1.40	17.22	4.809	4209	19.08	3178.8	2.9530	0.458	1.294	6664
1.50	18.22	4.488	4157	18.69	3299.0	2.9988	.469	1.293	6694
1.60	19.20	4.208	4091	18.30	3416.3	3.0419	.480	1.292	6711
1.70	20.16	3.960	4014	17.93	3530.8	3.0823	.490	1.292	6717
Percent fluorine in oxidant by weight, 78.08									
1.55	17.55	4.697	4333	18.59	3317.5	2.9700	0.460	1.303	6833
1.60	18.02	4.551	4298	18.40	3372.4	2.9890	.465	1.303	6841
1.65	18.48	4.413	4228	18.31	3426.7	3.0041	.470	1.300	6807
Percent fluorine in oxidant by weight, 79.67									
1.48	16.66	5.003	4418	18.89	3232.1	2.9282	0.450	1.305	6840
1.51	16.94	4.904	4402	18.78	3265.2	2.9399	.453	1.305	6848
1.55	17.31	4.777	4351	18.70	3309.0	2.9531	.457	1.303	6827
Percent fluorine in oxidant by weight, 80.15									
1.48	16.40	5.098	4440	18.98	3207.7	2.9157	0.447	1.306	6839
1.48	16.59	5.029	4431	18.91	3229.8	2.9236	.449	1.306	6846
1.50	16.77	4.962	4408	18.86	3251.8	2.9306	.451	1.305	6838
Percent fluorine in oxidant by weight, 81.46									
1.38	15.45	5.471	4498	19.32	3113.3	2.8700	0.436	1.309	6817
1.40	15.64	5.393	4493	19.25	3135.6	2.8783	.438	1.308	6828
1.42	15.83	5.317	4476	19.20	3157.7	2.8859	.440	1.308	6825
Percent fluorine in oxidant by weight, 82.61									
1.30	14.53	5.882	4527	19.65	3019.9	2.8241	0.425	1.312	6776
1.33	14.85	5.735	4528	19.53	3057.2	2.8386	.429	1.311	6799
1.40	15.48	5.462	4480	19.41	3131.0	2.8633	.436	1.307	6793
1.50	16.40	5.098	4395	19.23	3239.7	2.8965	.448	1.300	6772

^aThe base used for enthalpy is given in ref. 4.

^bParameters based on frozen composition.

TABLE III. - THEORETICAL ROCKET PERFORMANCE AT ASSIGNED EXIT TEMPERATURES FOR LIQUID METHANE WITH
SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion or compression from
combustion-chamber pressure of 600 lb/sq in. abs.]

(a) Percent fluorine in oxidant, 0 (100 percent oxygen)

Temperature, T, °K	Static pressure, P, lb/sq in. abs	Enthalpy, h, cal/g	Isentropic exponent, γ	Specific heat, c _p cal (g)(°K)	Absolute vis- cosity, μ, micro- poises	Thermal conduc- tivity, k, cal (cm)(sec)(°K)	Area ratio, ε	Thrust coeffi- cient, C _F	Specific impulse, I, lb-sec
r, 1.00; percent fuel, 20.04; O/F, 3.990									
3600	714.07	2699.4	1.200	0.5212	895	0.00056	---	0.652	115.5
3200	354.07	2492.4	1.204	0.5138	829	0.00052	1.00	0.995	176.3
2800	161.89	2288.6	1.208	0.5047	761	0.00047	1.26	0.954	220.1
2400	66.796	2089.0	1.214	0.4933	688	0.00041	2.09	1.242	255.7
2000	24.097	1894.5	1.222	0.4783	609	0.00036	4.16	1.443	285.8
1600	7.240	1707.1	1.234	0.4578	523	0.00030	9.90	1.613	328.6
1200	1.668	1529.4	1.254	0.4289	427	0.00023	29.56	1.759	311.7
900	.423	1404.8	1.277	0.4008	346	0.00018	82.96	1.855	343.5
600	.071	1289.4	1.309	0.3684	252	0.00012	317.07	1.939	343.5
r, 1.50; percent fuel, 24.58; O/F, 3.089									
3600	777.80	3325.6	1.205	0.5679	870	0.00049	---	0.590	109.2
3200	391.56	3100.0	1.209	0.5597	807	0.00045	1.02	0.954	176.8
2800	182.10	2878.0	1.214	0.5497	740	0.00041	1.19	1.209	224.0
2400	76.607	2660.6	1.220	0.5372	669	0.00036	1.91	1.414	261.9
2000	28.272	2448.8	1.228	0.5206	593	0.00031	3.68	1.514	293.8
1600	8.733	2244.9	1.241	0.4978	510	0.00025	8.50	1.613	321.1
1200	2.085	2051.9	1.262	0.4657	417	0.00019	24.44	1.734	339.0
900	.847	1916.7	1.286	0.4350	337	0.00015	56.20	1.830	354.7
600	.095	1791.2	1.318	0.4013	245	0.00010	242.19	1.915	354.7
r, 1.40; percent fuel, 25.98; O/F, 2.850									
3600	875.72	3551.9	1.208	0.5825	864	0.00061	---	0.498	92.9
3200	444.25	3320.5	1.212	0.5740	802	0.00056	1.09	0.904	168.6
2800	208.39	3092.9	1.217	0.5637	736	0.00051	1.12	1.173	218.7
2400	88.535	2869.9	1.223	0.5508	665	0.00045	1.74	1.386	258.3
2000	33.048	2652.8	1.232	0.5338	590	0.00039	3.29	1.563	291.4
1600	10.348	2443.7	1.245	0.5103	507	0.00032	7.46	1.714	319.6
1200	2.512	2245.8	1.266	0.4775	415	0.00025	21.01	1.813	337.9
900	.669	2107.2	1.290	0.4463	336	0.00019	55.96	1.900	354.1
600	.118	1978.3	1.322	0.4124	244	0.00013	200.88	1.900	354.1
r, 1.50; percent fuel, 27.32; O/F, 2.660									
3600	1034.4	3790.2	1.211	0.5967	860	0.00062	---	0.324	60.6
3200	529.34	3553.2	1.215	0.5880	798	0.00057	1.45	0.629	154.8
2800	250.76	3320.1	1.220	0.5774	732	0.00052	1.05	1.121	209.4
2400	107.73	3091.7	1.226	0.5641	663	0.00046	1.55	1.345	251.3
2000	40.739	2869.4	1.235	0.5466	587	0.00040	2.84	1.531	286.0
1600	12.952	2655.3	1.249	0.5226	505	0.00033	6.29	1.790	315.3
1200	3.202	2452.6	1.270	0.4892	413	0.00026	17.30	1.688	334.4
900	.866	2310.5	1.295	0.4578	335	0.00020	45.21	1.880	351.2
600	.156	2178.2	1.326	0.4239	244	0.00014	158.99	1.880	351.2
r, 1.60; percent fuel, 28.62; O/F, 2.493									
3200	658.21	3796.8	1.219	0.6016	795	0.00059	---	0.720	134.1
2800	315.14	3558.3	1.224	0.5907	730	0.00053	1.00	0.500	195.8
2400	137.03	3324.6	1.230	0.5771	660	0.00047	1.35	1.293	241.1
2000	52.543	3097.2	1.240	0.5592	586	0.00041	2.39	1.491	277.8
1600	16.978	2878.2	1.253	0.5348	504	0.00034	5.14	1.656	308.6
1200	4.278	2670.7	1.275	0.5009	413	0.00026	13.76	1.762	328.5
900	1.177	2525.0	1.299	0.4693	335	0.00020	35.24	1.856	346.0
600	.216	2389.3	1.330	0.4357	244	0.00014	121.26	1.856	346.0
r, 1.80; percent fuel, 31.09; O/F, 2.216									
3200	1105.3	4301.3	1.227	0.6279	792	0.00061	---	0.297	54.6
2800	540.68	4052.3	1.232	0.6164	727	0.00055	1.57	0.848	155.5
2400	240.90	3808.5	1.239	0.6022	658	0.00049	1.06	1.387	254.5
2000	94.990	3571.2	1.249	0.5837	584	0.00043	1.64	1.55	211.8
1600	31.710	3342.4	1.263	0.5585	503	0.00035	3.28	1.697	289.2
1200	8.301	3125.6	1.285	0.5242	412	0.00028	8.27	1.577	311.3
900	2.359	2973.0	1.309	0.4926	335	0.00021	20.27	1.803	330.6
600	.450	2830.1	1.338	0.4598	246	0.00015	66.74	1.803	330.6

TABLE III. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED EXIT TEMPERATURES FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion or compression from combustion-chamber pressure of 600 lb/sq in. abs.]

(b) Percent fluorine in oxidant by weight, 19.19

Temperature, T_e °K	Static pressure, P_e lb/sq in. abs	Enthalpy, h , cal/g	ISENTROPIC exponent, γ	Specific heat, c_p , cal (°K)	Absolute visco- cosity, μ , micro- poises	Thermal conduc- tivity, k , cal (cm)(sec) (°K)	Area ratio, ϵ	Thrust coeffi- cient, C_F	Specific impulse, I , lb-sec lb
$r, 1.20; \text{percent fuel, } 21.10; O/F, 3.740$									
4000	1034.9	3215.7	1.221	0.5270	1046	0.00068	---	---	---
3600	580.20	3006.1	1.234	0.5299	975	0.00068	2.60	0.169	31.7
3200	336.35	28799.1	1.228	0.5136	901	0.00057	1.01	.735	117.9
2800	180.27	2595.4	1.233	0.5147	823	0.00051	1.289	1.282	191.7
2400	67.048	2395.7	1.229	0.4990	782	0.00045	1.240	1.240	183.6
2000	26.064	2020.3	1.229	0.4790	689	0.00039	1.276	1.271	183.6
1600	8.904	18034.7	1.223	0.4592	587	0.00035	1.372	1.376	183.6
1200	2.761	1708.9	1.207	0.4310	452	0.00026	2.155	1.710	183.6
900	.651	1708.9	1.207	0.4056	363	0.00019	5.435	1.799	337.5
$r, 1.40; \text{percent fuel, } 23.76; O/F, 3.208$									
3600	660.58	3194.0	1.227	0.5492	956	0.00065	---	---	---
3200	350.70	3061.1	1.231	0.5414	883	0.00059	1.00	0.661	26.3
2800	173.03	20561.1	1.236	0.5320	807	0.00053	1.21	.974	186.1
2400	77.787	2750.5	1.242	0.5202	727	0.00047	1.37	1.205	230.1
2000	30.965	2545.4	1.252	0.5047	641	0.00040	1.306	1.368	266.1
1600	10.440	2247.6	1.266	0.4835	548	0.00033	1.16	1.593	289.7
1200	2.761	2159.7	1.287	0.4545	445	0.00026	1.65	1.692	223.1
900	.791	2027.3	1.311	0.4277	358	0.00020	4.634	1.782	440.4
$r, 1.50; \text{percent fuel, } 25.05; O/F, 2.992$									
3600	742.44	3600.1	1.228	0.5629	948	0.00066	---	---	---
3200	395.86	3176.5	1.233	0.5548	877	0.00060	1.03	0.586	112.3
2800	196.27	3156.5	1.238	0.5451	802	0.00054	1.14	.929	178.2
2400	88.732	2040.8	1.244	0.5329	722	0.00048	1.71	1.172	224.8
2000	35.554	20730.7	1.254	0.5170	637	0.00041	1.06	1.368	262.3
1600	12.088	20528.0	1.268	0.4953	548	0.00034	6.42	1.533	294.0
1200	3.226	20335.5	1.290	0.4656	442	0.00026	16.50	1.675	321.2
900	.932	2199.9	1.314	0.4384	358	0.00020	4.057	1.769	339.1
$r, 1.60; \text{percent fuel, } 26.28; O/F, 2.805$									
3600	862.51	3814.7	1.231	0.5762	942	0.00067	1.13	0.468	89.7
3200	468.25	3585.8	1.235	0.5679	871	0.00061	1.07	.867	166.2
2800	230.51	3060.6	1.240	0.5578	797	0.00055	1.07	1.126	214.4
2400	104.91	31359.9	1.247	0.5453	718	0.00049	1.55	1.186	256.0
2000	42.363	20244.9	1.257	0.5290	634	0.00042	2.71	1.335	297.1
1600	14.582	20217.5	1.271	0.5068	544	0.00035	5.60	1.507	329.1
1200	3.928	2020.6	1.293	0.4766	441	0.00026	14.17	1.655	317.4
900	1.144	20381.6	1.317	0.4491	358	0.00020	3.442	1.751	358.4
$r, 1.80; \text{percent fuel, } 28.82; O/F, 2.495$									
3600	684.23	4024.8	1.241	0.5934	864	0.00064	1.00	0.672	127.7
3200	345.74	3780.6	1.246	0.5864	790	0.00057	1.00	1.003	190.7
2800	159.76	36559.7	1.253	0.5669	716	0.00051	1.83	1.223	206.4
2400	85.680	35544.7	1.263	0.5583	639	0.00045	2.03	1.283	247.8
2000	38.980	30118.1	1.278	0.5293	558	0.00036	4.02	1.328	287.1
1600	6.356	20118.3	1.300	0.4983	438	0.00028	9.79	1.601	304.4
1200	1.809	27665.9	1.323	0.4706	354	0.00020	3.113	1.706	324.5
(c) Percent fluorine in oxidant by weight, 37.25									
$r, 1.30; \text{percent fuel, } 20.35; O/F, 3.915$									
4000	828.94	3271.0	1.244	0.5088	1163	0.00074	1.21	0.492	81.9
3600	486.36	3068.7	1.248	0.5029	1080	0.00068	1.03	.799	155.2
3200	270.01	2868.9	1.252	0.4960	994	0.00062	1.03	1.045	203.0
2800	139.97	2672.1	1.258	0.4876	904	0.00055	1.39	1.840	240.9
2400	66.513	2479.0	1.265	0.4773	809	0.00049	2.01	1.840	287.8
2000	28.192	2290.7	1.275	0.4638	708	0.00042	3.49	1.547	320.4
1600	10.215	2108.6	1.291	0.4456	601	0.00034	7.01	1.547	320.4
1200	3.935	10351.1	1.311	0.4218	483	0.00026	16.92	1.671	324.6
900	.908	1811.9	1.334	0.3994	386	0.00020	3.935	1.754	340.7
$r, 1.50; \text{percent fuel, } 22.77; O/F, 3.591$									
4000	953.46	3633.8	1.245	0.5355	1136	0.00076	1.88	0.244	47.9
3600	559.97	3430.9	1.249	0.5292	1056	0.00070	1.88	0.730	143.6
3200	311.25	3210.7	1.253	0.5218	973	0.00064	1.83	1.000	196.5
2800	161.59	3033.7	1.259	0.5120	895	0.00057	1.83	1.207	137.2
2400	76.929	2880.7	1.266	0.5018	793	0.00050	1.84	1.379	187.1
2000	32.686	2602.7	1.276	0.4875	695	0.00043	3.16	1.528	200.0
1600	11.882	2411.4	1.291	0.4681	590	0.00035	6.28	1.657	225.6
1200	3.431	2289.1	1.313	0.4420	475	0.00027	15.04	1.742	242.4
900	1.060	2099.6	1.336	0.4193	380	0.00021	3.472	1.742	342.4
$r, 1.60; \text{percent fuel, } 23.93; O/F, 3.179$									
3600	684.14	3606.5	1.250	0.5418	1047	0.00071	1.00	0.670	31.9
3200	347.56	3391.3	1.254	0.5342	964	0.00065	1.00	.961	189.3
2800	180.83	3179.4	1.260	0.5250	878	0.00058	1.17	1.179	132.2
2400	86.307	30271.6	1.267	0.5137	787	0.00051	1.72	1.358	166.7
2000	36.781	28768.9	1.277	0.4985	690	0.00044	2.92	1.491	223.4
1600	15.420	28573.1	1.292	0.4790	586	0.00036	5.75	1.511	199.7
1200	5.893	28486.6	1.314	0.4525	473	0.00028	13.66	1.644	193.8
900	1.807	28550.7	1.337	0.4289	379	0.00021	3.136	1.732	341.1
$r, 1.70; \text{percent fuel, } 25.05; O/F, 2.992$									
3600	711.74	3798.1	1.251	0.5542	1039	0.00072	1.03	0.586	115.4
3200	397.32	3578.0	1.256	0.5463	957	0.00066	1.03	.911	179.3
2800	207.38	33146.3	1.269	0.5359	872	0.00059	1.58	1.443	225.1
2400	99.279	31486.3	1.279	0.5101	686	0.00045	3.65	1.333	166.2
2000	42.477	29041.6	1.294	0.4897	583	0.00037	5.16	1.491	223.4
1600	15.572	28741.4	1.316	0.4687	470	0.00028	12.16	1.628	220.5
1200	4.543	25500.7	1.339	0.4391	377	0.00022	2.770	1.719	336.3
900	1.416	2415.4	1.360	0.4361	272	0.00016	60.97	1.774	346.4
$r, 1.80; \text{percent fuel, } 27.19; O/F, 2.677$									
3600	979.82	4195.2	1.254	0.5782	1027	0.00074	1.00	0.274	53.6
3200	550.10	3965.5	1.259	0.5696	946	0.00068	1.70	.769	150.1
2800	289.12	37379.5	1.265	0.5598	862	0.00061	1.01	1.047	204.4
2400	139.61	3618.0	1.272	0.5475	774	0.00054	1.32	1.261	246.1
2000	60.317	34080.5	1.283	0.5317	679	0.00046	2.11	1.437	280.6
1600	22.367	30934.4	1.298	0.5108	578	0.00038	4.00	1.587	309.9
1200	6.614	28945.4	1.321	0.4888	467	0.00029	9.18	1.686	329.8
900	2.088	28753.2	1.343	0.4588	376	0.00023	20.55	1.774	346.4
600	.445	2619.0	1.360	0.4361	272	0.00016	60.97	1.774	346.4

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TABLE III. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED EXIT TEMPERATURES FOR LIQUID
METHANE WITH SEVERAL FLUORINE OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion or compression from
combustion-chamber pressure of 600 lb/sq in. abs.]

(d) Percent fluorine in oxidant by weight, 54.29

Temper- ature, T, °K	Static pressure, P, lb/sq in. abs	Enthalpy, h, cal/g	Isentropic exponent, γ	Specific heat, c _p , cal (°K)	Absolute vis- cosity, μ, dynes cm ⁻² msec ⁻¹	Thermal condi- civity, k, cal (cm)(mec) (°K)	Area ratio, ε	Thrust coeffi- cient, C _T	Specific impulse, I, lb-sec lb
r, 1.50; percent fuel, 18.26; O/F, 4.475									
4000	631.23	3121.1	1.270	0.4764	1380	0.00050	1.02	0.608	121.3
3600	585.83	3051.6	1.274	0.4709	1221	0.00073	1.06	0.633	176.0
3200	524.06	2974.4	1.279	0.4646	1117	0.00066	1.08	0.653	216.9
2800	122.09	2556.0	1.285	0.4571	1010	0.00059	1.40	1.287	250.6
2400	61.351	2479.0	1.293	0.4479	898	0.00052	2.07	1.256	305.1
2000	27.708	2302.0	1.303	0.4359	781	0.00044	3.43	1.402	379.6
1600	10.800	2030.8	1.318	0.4200	657	0.00036	6.44	1.530	305.1
1200	3.379	1666.8	1.340	0.3992	525	0.00028	14.45	1.735	324.9
900	1.117	1749.7	1.362	0.3816	215	0.00021	34.15	1.773	342.9
600	.251	1637.6	1.384	0.3656	296	0.00015	88.76	1.789	366.8
r, 1.40; percent fuel, 19.40; O/F, 4.156									
4000	662.09	3879.2	1.269	0.4890	1302	0.00081	1.04	0.577	115.8
3600	504.03	3084.7	1.273	0.4834	1204	0.00074	1.06	0.655	173.8
3200	234.21	2698.6	1.278	0.4769	1103	0.00067	1.37	1.075	229.8
2800	127.38	2703.4	1.284	0.4691	997	0.00060	1.67	1.285	265.8
2400	65.873	2517.5	1.291	0.4598	887	0.00053	2.04	1.396	300.3
2000	21.192	2160.4	1.317	0.407	649	0.00036	6.29	1.526	306.3
1600	7.493	1699.2	1.340	0.4092	518	0.00028	14.07	1.641	329.3
1200	1.183	1877.2	1.361	0.3908	411	0.00021	30.54	1.718	344.8
900	.259	1757.5	1.383	0.3743	293	0.00015	87.01	1.788	359.0
r, 1.50; percent fuel, 20.50; O/F, 3.879									
4000	706.24	3441.1	1.268	0.5014	1285	b. 0.00081	1.07	0.570	106.9
3600	549.50	3044.2	1.272	0.4955	1282	0.00075	1.04	0.638	169.0
3200	249.50	2650.8	1.277	0.4889	1189	0.00069	1.33	1.057	213.8
2800	135.53	2850.8	1.283	0.4809	984	0.00060	1.65	1.255	249.0
2400	67.833	2647.4	1.291	0.4710	878	0.00053	2.22	1.387	279.6
2000	30.528	2160.4	1.317	0.4582	764	0.00045	5.05	1.519	306.4
1600	11.696	1699.4	1.340	0.4190	643	0.00037	13.52	1.636	329.9
1200	2.819	1877.2	1.361	0.4000	513	0.00028	39.34	1.714	345.7
900	.274	1851.9	1.383	0.3831	291	0.00015	83.57	1.786	360.4
r, 1.60; percent fuel, 21.57; O/F, 3.438									
4000	766.30	3607.4	1.268	0.5135	1270	0.00082	1.15	0.463	93.6
3600	616.93	3403.2	1.272	0.5075	1176	0.00076	1.02	0.503	168.2
3200	270.26	3201.6	1.277	0.5005	1078	0.00069	1.28	1.032	208.8
2800	146.77	3002.9	1.283	0.4923	976	0.00061	1.66	1.217	246.1
2400	73.482	2808.0	1.291	0.4821	869	0.00054	2.05	1.373	277.7
2000	33.056	2617.7	1.301	0.4689	757	0.00046	3.55	1.535	307.7
1600	14.020	2357.3	1.320	0.4384	658	0.00039	7.76	1.629	329.4
1200	4.003	2120.4	1.341	0.4094	505	0.00029	12.65	1.709	345.6
900	1.200	2011.4	1.361	0.3904	405	0.00022	27.65	1.782	360.4
600	.297	1920.0	1.383	0.3720	290	0.00015	79.68	1.782	360.4
r, 1.60; percent fuel, 23.65; O/F, 3.232									
4000	949.09	3853.8	1.268	0.5135	1270	0.00082	2.54	0.178	36.0
3600	578.65	3740.2	1.273	0.5036	1204	0.00078	1.00	0.651	190.0
3200	335.21	3252.0	1.278	0.5232	1059	0.00070	1.45	1.165	235.4
2800	182.45	2922.8	1.284	0.5124	957	0.00063	1.84	1.334	269.7
2400	81.83	2512.8	1.292	0.4936	855	0.00055	2.24	1.480	299.1
2000	21.197	2161.9	1.318	0.4897	746	0.00047	3.12	1.607	324.7
1600	16.039	2129.7	1.318	0.4713	629	0.00039	4.90	1.680	341.9
1200	5.017	2154.3	1.341	0.4475	504	0.00030	10.81	1.692	357.3
900	1.659	2141.8	1.362	0.4276	401	0.00023	16.00	1.693	356.7
600	.374	2126.5	1.384	0.4099	288	0.00016	69.93	1.765	357.3
(e) Percent fluorine in oxidant by weight, 70.37									
r, 1.40; percent fuel, 17.22; O/F, 4.808									
4000	730.04	3466.7	1.268	0.5371	1244	0.00085	2.54	0.178	36.0
4000	479.98	3053.4	1.296	0.4559	1478	0.00087	1.20	0.749	155.8
3600	303.43	3219.0	1.278	0.5088	1361	0.00070	1.00	0.651	199.8
3200	188.83	2722.8	1.305	0.4451	1239	0.00071	1.15	0.962	234.4
2800	103.78	2546.1	1.312	0.4383	1124	0.00063	1.51	1.133	264.4
2400	54.588	2178.4	1.320	0.4298	985	0.00055	2.16	1.279	294.1
2000	25.967	2020.6	1.331	0.4190	850	0.00047	3.16	1.404	323.6
1600	10.745	1907.6	1.350	0.3965	725	0.00039	5.00	1.603	336.3
1200	3.665	1790.4	1.369	0.3865	600	0.00029	13.00	1.603	350.7
900	1.266	1765.6	1.389	0.3720	440	0.00023	26.61	1.603	350.7
600	.303	1655.9	1.407	0.3602	312	0.00015	70.88	1.758	364.0
r, 1.60; percent fuel, 18.22; O/F, 4.488									
4000	771.99	3413.6	1.291	0.4723	1573	0.00095	1.32	0.384	79.9
4000	506.70	3225.7	1.295	0.4674	1400	0.00098	1.32	0.223	150.4
3600	319.78	3039.6	1.299	0.4621	1344	0.00090	1.00	0.651	191.7
3200	162.27	2856.0	1.304	0.4562	1236	0.00082	1.43	1.123	233.0
2800	83.94	2657.0	1.310	0.4421	1102	0.00064	1.87	1.270	264.2
2400	55.152	2467.0	1.318	0.4240	974	0.00056	2.12	1.403	291.1
2000	27.117	2182.0	1.328	0.4292	841	0.00047	3.38	1.517	315.6
1600	13.190	2154.8	1.345	0.4144	702	0.00038	6.04	1.622	337.8
1200	3.743	1909.2	1.368	0.3957	595	0.00029	12.69	1.622	351.5
900	1.311	1875.6	1.388	0.3806	437	0.00022	26.03	1.622	365.5
600	.315	1763.3	1.406	0.3685	309	0.00016	69.48	1.757	365.5
r, 1.60; percent fuel, 19.20; O/F, 4.208									
4000	828.45	3554.9	1.289	0.4837	1554	0.00096	1.62	0.296	61.7
4000	543.03	3372.5	1.293	0.4787	1443	0.00089	1.00	0.684	142.8
3600	3442.17	3182.1	1.298	0.4732	1329	0.00081	1.10	0.919	191.7
3200	205.47	2904.0	1.303	0.4670	1211	0.00073	1.42	1.103	229.9
2800	115.20	2606.6	1.309	0.4597	1090	0.00065	2.04	1.257	262.2
2400	60.578	2262.4	1.317	0.4508	954	0.00057	3.25	1.392	290.2
2000	26.834	2144.8	1.328	0.4392	833	0.00048	4.25	1.530	317.2
1600	13.875	2075.6	1.344	0.4241	702	0.00039	7.50	1.616	337.2
1200	3.946	1950.7	1.367	0.4057	550	0.00029	15.00	1.616	357.2
900	1.306	1920.7	1.387	0.3992	433	0.00023	28.06	1.616	357.2
600	.333	1875.9	1.405	0.3767	307	0.00016	66.97	1.755	366.1
r, 1.70; percent fuel, 20.18; O/F, 3.980									
4000	901.96	3720.8	1.289	0.4950	1537	0.00097	3.81	0.118	24.7
4000	590.64	3523.8	1.293	0.4897	1427	0.00096	3.81	0.635	132.5
3600	371.81	3182.0	1.297	0.4841	1318	0.00082	1.07	0.880	165.5
3200	223.04	3136.7	1.302	0.4777	1199	0.00074	1.07	0.980	204.4
2800	126.01	2817.1	1.308	0.4700	1079	0.00066	1.47	1.240	238.8
2400	65.927	2578.6	1.313	0.4637	955	0.00057	2.05	1.379	268.8
2000	31.301	2402.9	1.324	0.4590	826	0.00049	3.09	1.379	287.8
1600	10.835	2142.9	1.344	0.4333	690	0.00039	5.51	1.501	313.4
1200	4.279	2023.6	1.366	0.4135	546	0.00030	11.57	1.610	

TABLE III. - Continued. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED EXIT TEMPERATURES FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion or compression from combustion-chamber pressure of 600 lb/sq in. abs.]

(f) Percent fluorine in oxidant by weight, 78.08

Temper- ature, °K	Static pressure, lb/sq in. abs	Enthalpy, h, cal/g	Isentropic exponent, γ	Specific heat, c_p , cal (°K)	Absolute vis- cosity, c micro- poises (cm (sec)) 10 ⁻⁴	Thermal conduc- tivity, k cal cm ² sec ⁻¹	Area ratio, r	Thrust/ coeffi- cient, G	Specific impulse, I _s , lb-sec lb
r, 1.55; percent fuel, 17.55; O/F, 4.687									
4400	641.13	3348.4	1.302	0.460	1658	0.00099	-----	0.542	175.1
4000	426.10	3165.1	1.306	0.4560	1536	0.00091	1.07	0.542	175.1
3600	273.54	2983.7	1.311	0.4510	1411	0.00083	1.08	0.502	170.3
3200	186.37	2804.4	1.316	0.4452	1283	0.00074	1.08	0.905	211.3
2800	127.77	2625.0	1.320	0.4386	1155	0.00066	1.57	1.194	284.0
2400	91.78	2445.5	1.324	0.4326	1016	0.00057	2.25	1.291	374.1
2000	64.79	2266.0	1.328	0.4267	876	0.00049	3.53	1.412	599.0
1600	40.47	2119.4	1.332	0.4188	787	0.00040	5.53	1.552	938.0
1200	19.60	1959.5	1.336	0.4088	572	0.00030	10.74	1.652	1393.7
900	1.291	1845.1	1.339	0.3745	449	0.00023	25.59	1.668	337.9
r, 1.60; percent fuel, 18.08; O/F, 4.551									
4400	665.55	3419.7	1.302	0.4661	1650	0.00099	-----	0.536	109.7
4000	440.71	3234.2	1.306	0.4623	1512	0.00091	1.10	0.536	109.7
3600	281.70	3050.7	1.310	0.4562	1405	0.00083	1.18	0.584	160.3
3200	171.81	2869.3	1.315	0.4505	1279	0.00075	1.18	0.584	202.8
2800	96.84	2689.4	1.320	0.4437	1147	0.00066	1.54	1.146	242.6
2400	58.78	2514.6	1.324	0.4353	1011	0.00058	2.81	1.285	373.2
2000	35.25	2330.5	1.328	0.4265	871	0.00049	3.47	1.408	595.3
1600	19.28	2147.5	1.332	0.4177	787	0.00040	6.10	1.518	938.7
1200	3.702	2014.8	1.336	0.4076	572	0.00030	12.50	1.616	1393.7
900	1.327	1819.1	1.339	0.3747	447	0.00023	25.12	1.684	358.0
r, 1.65; percent fuel, 18.48; O/F, 4.415									
4400	773.16	3507.6	1.298	0.4783	1632	0.00099	-----	0.556	96.5
4000	472.09	3324.1	1.307	0.4733	1593	0.00091	1.18	0.785	139.7
3600	300.70	3143.6	1.312	0.4681	1504	0.00083	1.00	0.761	202.6
3200	188.72	2950.1	1.316	0.4621	1454	0.00075	1.07	0.775	260.7
2800	104.70	2767.9	1.321	0.4541	1319	0.00066	1.50	1.019	216.5
2400	55.66	2581.0	1.327	0.4465	1201	0.00058	2.75	1.175	380.7
2000	26.805	2414.6	1.330	0.4395	1063	0.00049	3.37	1.301	586.4
1600	11.353	2230.5	1.334	0.4305	918	0.00030	5.95	1.514	930.3
1200	3.437	2048.5	1.336	0.4206	787	0.00020	10.76	1.615	1391.6
900	1.335	1855.4	1.341	0.3748	447	0.00016	25.49	1.748	358.8
(g) Percent fluorine in oxidant by weight, 79.87									
r, 1.48; percent fuel, 16.88; O/F, 5.008									
4400	857.06	3404.8	1.301	0.4544	1808	0.00106	3.66	0.184	26.3
4000	589.77	3224.1	1.306	0.4495	1562	0.00090	1.03	0.202	217.6
3600	399.02	3045.8	1.310	0.4430	1424	0.00082	1.04	0.212	247.9
3200	252.45	2868.8	1.314	0.4341	1304	0.00074	1.23	0.219	216.9
2800	154.65	2689.3	1.319	0.4247	1169	0.00065	1.63	2.170	348.8
2400	89.437	2502.0	1.326	0.4153	1021	0.00057	2.33	1.303	576.9
2000	48.379	2318.6	1.330	0.4056	887	0.00048	3.66	1.420	801.9
1600	26.936	2133.1	1.336	0.3966	752	0.00039	6.26	1.528	1344.3
1200	10.343	1947.8	1.339	0.3879	615	0.00020	11.86	1.628	358.8
900	3.437	1755.9	1.342	0.3665	454	0.00016	25.64	1.747	371.3
r, 1.51; percent fuel, 18.84; O/F, 4.204									
4800	870.94	3446.5	1.301	0.4577	1603	0.00100	1.69	0.338	98.8
4400	599.02	3264.4	1.305	0.4527	1561	0.00090	1.04	0.390	128.8
4000	399.84	3084.2	1.310	0.4482	1427	0.00082	1.04	0.331	186.8
3600	256.14	2905.9	1.314	0.4333	1300	0.00074	1.03	0.311	218.9
3200	136.69	2728.9	1.319	0.4238	1166	0.00065	1.23	0.314	248.4
2800	80.629	2549.5	1.324	0.4138	1021	0.00057	1.92	0.330	376.8
2400	42.379	2365.6	1.330	0.4036	887	0.00048	3.28	0.328	501.9
2000	21.936	2181.6	1.334	0.3936	752	0.00039	6.26	0.328	1021.2
1600	10.045	2002.1	1.338	0.3839	615	0.00020	11.86	0.328	1444.8
1200	3.473	1819.5	1.342	0.3630	454	0.00016	25.64	0.386	358.8
r, 1.55; percent fuel, 17.31; O/F, 4.777									
4400	629.39	3433.8	1.302	0.4575	1659	0.00099	1.06	0.556	118.0
4000	418.37	3149.1	1.307	0.4529	1548	0.00091	1.02	0.511	1212.0
3600	267.69	2968.9	1.311	0.4482	1400	0.00082	1.04	0.580	186.8
3200	171.44	2789.7	1.316	0.4333	1269	0.00074	1.03	0.581	212.0
2800	98.00	2605.9	1.321	0.4238	1130	0.00065	1.21	0.581	243.7
2400	50.609	2422.6	1.326	0.4138	998	0.00056	1.61	1.167	348.4
2000	26.656	2238.4	1.330	0.4038	858	0.00048	2.32	1.300	576.8
1600	13.045	2054.9	1.334	0.3939	713	0.00039	4.67	1.402	1021.2
1200	3.473	1869.5	1.338	0.3832	578	0.00020	11.86	0.328	1444.8
900	1.273	1683.0	1.340	0.3722	450	0.00013	25.64	0.386	358.8
(h) Percent fluorine in oxidant by weight, 80.15									
r, 1.46; percent fuel, 18.40; O/F, 5.098									
4800	838.04	3169.8	1.302	0.4511	1817	0.00106	2.48	0.186	39.5
4400	577.83	3189.5	1.306	0.4468	1694	0.00098	1.02	0.214	179.1
4000	385.31	3012.8	1.311	0.4418	1569	0.00090	1.02	0.244	179.1
3600	947.60	2836.4	1.315	0.4370	1441	0.00082	1.04	0.287	212.7
3200	152.89	2666.2	1.320	0.4317	1309	0.00074	1.24	1.024	217.8
2800	84.874	2489.4	1.324	0.4253	1174	0.00065	1.64	1.175	249.7
2400	47.280	2318.6	1.329	0.4174	1038	0.00057	2.35	1.305	377.5
2000	23.026	2137.6	1.333	0.4076	898	0.00048	3.66	1.422	502.3
1600	10.314	1957.5	1.338	0.3978	752	0.00039	6.26	1.526	1021.2
1200	3.420	1774.5	1.342	0.3872	615	0.00020	11.86	0.328	1444.8
900	1.230	1581.0	1.343	0.3764	454	0.00016	25.64	0.386	358.8
r, 1.48; percent fuel, 18.88; O/F, 5.028									
4800	845.74	3194.8	1.303	0.4533	1813	0.00106	2.80	0.163	37.7
4400	588.33	3195.9	1.306	0.4484	1691	0.00098	1.03	0.202	217.8
4000	388.57	3037.5	1.310	0.4439	1566	0.00090	1.04	0.202	179.8
3600	249.60	2856.0	1.315	0.4337	1307	0.00082	1.24	1.028	217.8
3200	110.05	2686.6	1.320	0.4287	1178	0.00074	1.63	1.173	249.6
2800	68.597	2514.6	1.324	0.4234	1035	0.00065	2.32	1.304	377.5
2400	41.597	2344.6	1.328	0.4134	903	0.00057	3.66	1.422	502.3
2000	21.197	2164.6	1.332	0.4036	767	0.00048	6.26	1.526	1021.2
1600	9.870	1977.7	1.336	0.3937	619	0.00039	11.86	0.328	1444.8
1200	3.420	1791.7	1.338	0.3834	454	0.00020	25.64	0.386	358.8
900	1.230	1603.0	1.341	0.3721	321	0.00016	27.77	1.746	371.3
r, 1.50; percent fuel, 18.77; O/F, 4.882									
4800	868.64	3429.5	1.301	0.4557	1808	0.00106	2.43	0.083	27.6
4400	595.41	3248.2	1.305	0.4507	1686	0.00098	1.03	0.194	182.2
4000	326.86	3065.9	1.310	0.4448	1562	0.00090	1.03	0.233	177.1
3600	185.13	2894.1	1.315	0.4370	1435	0.00082	1.24	1.026	217.8
3200	102.94	2724.5	1.319	0.4326	1296	0.00074	1.63	1.173	249.6
2800	48.356	2544.6	1.323	0.4274	1056	0.00065	2.32</		

TABLE III. - Concluded. THEORETICAL ROCKET PERFORMANCE AT ASSIGNED EXIT TEMPERATURES FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion or compression from combustion-chamber pressure of 600 lb/sq in. abs.]

(i) Percent fluorine in oxidant weight, 81.46

Temperature, °F °K	Static pressure, P, lb/sq in. abs	Enthalpy h, cal/g	Isentropic exponent, γ	Specific heat, cp, cal (g)(°K)	Absolute vis- cosity, μ, micro- poises	Thermal conduc- tivity, k, cal (cm)(sec)(°K)	Area ratio, ε	Thrust coeffi- cient, C _T	Specific impulse, I, lb-sec lb
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r, 1.38; percent fuel, 15.45; o/F, 5.471

4800	793	.22	3.245	.5	1.306	0.4394	18.43	0.00105	-----
4400	646	.69	3.070	.7	1.310	0.4304	17.18	0.00097	1.68
4000	546	1.16	2.897	.7	1.314	0.4304	15.91	0.00089	1.01
3600	236	1.15	2.726	.4	1.318	0.4259	14.61	0.00081	1.05
3200	145	1.43	2.557	.1	1.324	0.4207	1.327	0.00073	1.27
2800	84	5.53	2.390	.0	1.330	0.4146	1.190	0.00065	1.67
2400	245	6.77	2.225	.56	1.338	0.4070	1.049	0.00056	2.40
2000	391	6.78	2.064	.7	1.342	0.3978	9.08	0.00047	3.75
1600	588	1.08	1.904	.7	1.365	0.3844	7.49	0.00038	6.53
12000	345	1.75	1.757	.5	1.387	0.3683	5.89	0.00029	13.24
900	1.215	1.648	1.648	.9	1.406	0.3559	4.61	0.00022	26.28
600	1.305	1.543	1.543	.6	1.422	0.3468	3.25	0.00015	67.62

r, 1.40; percent fuel, 15.64; o/F, 5.393

4800	794	.70	3.270	.3	1.305	0.4416	18.39	0.00105	-----
4400	448	.87	3.094	.7	1.309	0.4369	17.15	0.00097	1.71
4000	445	1.45	2.920	.6	1.314	0.4386	15.88	0.00089	1.01
3600	245	1.45	2.748	.7	1.318	0.4288	14.58	0.00081	1.05
3200	145	1.87	2.578	.5	1.323	0.4166	13.25	0.00073	1.27
2800	84	8.00	2.410	.6	1.349	0.4090	10.47	0.00056	1.67
2400	245	7.20	2.245	.4	1.348	0.3991	9.00	0.00048	1.75
2000	345	7.39	2.083	.7	1.349	0.3862	7.48	0.00039	6.53
1600	588	1.926	1.926	.5	1.365	0.3701	5.87	0.00029	26.84
12000	345	1.775	1.775	.2	1.387	0.3575	4.60	0.00022	26.31
900	1.215	1.666	1.666	.0	1.406	0.3484	3.24	0.00015	67.57
600	1.305	1.560	1.560	.3	1.421	0.3484	3.24	0.00015	1.745

r, 1.42; percent fuel, 15.85; o/F, 5.317

4800	808	.31	3.300	.7	1.304	0.4440	18.35	0.00105	-----
4400	557	.70	3.124	.1	1.308	0.4391	17.11	0.00097	1.86
4000	372	.96	2.949	.3	1.312	0.4348	15.84	0.00089	1.01
3600	240	1.14	2.776	.5	1.317	0.4302	14.55	0.00081	1.05
3200	147	1.63	2.605	.3	1.322	0.4249	13.22	0.00073	1.27
2800	666	1.667	2.436	.5	1.328	0.4187	11.85	0.00065	1.66
2400	146	1.82	2.270	.5	1.337	0.4110	10.44	0.00056	1.38
2000	345	1.585	1.908	.1	1.348	0.4010	9.98	0.00048	17.73
1600	588	1.647	1.650	.1	1.364	0.3880	7.46	0.00039	6.50
12000	338	1.798	1.798	.1	1.386	0.3717	5.86	0.00029	13.23
900	1.217	1.688	1.688	.0	1.405	0.3591	4.59	0.00022	1.33
600	1.305	1.588	1.588	.0	1.420	0.3498	3.23	0.00015	67.70

(j) Percent fluorine in oxidant by weight, 82.61

4800	808	.31	3.300	.7	1.304	0.4440	18.35	0.00105	-----
4400	557	.70	3.124	.1	1.308	0.4391	17.11	0.00097	1.86
4000	372	.96	2.949	.3	1.312	0.4348	15.84	0.00089	1.01
3600	240	1.14	2.776	.5	1.317	0.4302	14.55	0.00081	1.05
3200	147	1.63	2.605	.3	1.322	0.4249	13.22	0.00073	1.27
2800	666	1.667	2.436	.5	1.328	0.4187	11.85	0.00065	1.66
2400	146	1.82	2.270	.5	1.337	0.4110	10.44	0.00056	1.38
2000	345	1.585	1.908	.1	1.348	0.4010	9.98	0.00048	17.73
1600	588	1.647	1.650	.1	1.364	0.3880	7.46	0.00038	6.50
12000	338	1.798	1.798	.1	1.386	0.3717	5.86	0.00029	13.23
900	1.217	1.688	1.688	.0	1.405	0.3591	4.59	0.00022	1.33
600	1.305	1.588	1.588	.0	1.420	0.3498	3.23	0.00015	67.70

r, 1.30; percent fuel, 14.53; o/F, 5.682

4800	806	.31	3.300	.7	1.304	0.4440	18.35	0.00105	-----
4400	557	.70	3.124	.1	1.308	0.4391	17.11	0.00097	1.86
4000	372	.96	2.949	.3	1.312	0.4348	15.84	0.00089	1.01
3600	240	1.14	2.776	.5	1.317	0.4302	14.55	0.00081	1.05
3200	147	1.63	2.605	.3	1.322	0.4249	13.22	0.00073	1.27
2800	666	1.667	2.436	.5	1.328	0.4187	11.85	0.00065	1.66
2400	146	1.82	2.270	.5	1.337	0.4110	10.44	0.00056	1.38
2000	345	1.585	1.908	.1	1.348	0.4010	9.98	0.00048	17.73
1600	588	1.647	1.650	.1	1.364	0.3880	7.46	0.00038	6.50
12000	338	1.798	1.798	.1	1.386	0.3717	5.86	0.00029	13.23
900	1.217	1.688	1.688	.0	1.405	0.3591	4.59	0.00022	1.33
600	1.305	1.588	1.588	.0	1.420	0.3498	3.23	0.00015	67.70

r, 1.355; percent fuel, 14.85; o/F, 5.735

4800	768	.12	3.174	.3	1.308	0.4518	18.60	0.00104	-----
4400	532	.01	3.000	.6	1.313	0.4572	17.34	0.00096	1.51
4000	357	.25	2.832	.0	1.317	0.4521	16.06	0.00088	1.01
3600	231	.04	2.664	.0	1.321	0.4486	14.74	0.00080	1.05
3200	148	.71	2.497	.7	1.326	0.4436	13.39	0.00072	1.28
2800	83	1.250	2.333	.4	1.333	0.4407	12.01	0.00064	1.68
2400	45	1.37	2.171	.7	1.341	0.4053	10.58	0.00056	2.41
2000	22	2.16	2.013	.5	1.352	0.3907	9.10	0.00047	3.75
1600	9	5.55	1.859	.6	1.368	0.3783	7.56	0.00038	6.52
12000	3	3.355	1.711	.3	1.390	0.3627	5.94	0.00029	13.14
900	1	2.225	1.604	.3	1.409	0.3506	4.65	0.00022	25.97
600	.309	1.500	1.423	.0	1.423	0.3420	3.28	0.00015	66.33

r, 1.40; percent fuel, 15.48; o/F, 5.462

4800	806	.40	3.271	.4	1.303	0.4401	18.39	0.00104	-----
4400	555	.98	3.096	.4	1.308	0.4353	17.14	0.00097	1.82
4000	371	.52	2.923	.0	1.312	0.4309	15.87	0.00089	1.01
3600	239	.03	2.751	.6	1.316	0.4263	14.57	0.00081	1.05
3200	146	.82	2.588	.1	1.321	0.4211	13.84	0.00073	1.28
2800	85	1.119	2.414	.0	1.326	0.4149	11.87	0.00064	1.67
2400	45	1.840	2.250	.4	1.332	0.4072	10.45	0.00056	2.39
2000	22	3.393	2.089	.4	1.347	0.3974	8.99	0.00047	3.76
1600	9	5.55	1.939	.9	1.363	0.3845	7.47	0.00038	6.57
12000	3	3.191	1.788	.3	1.385	0.3683	5.86	0.00029	13.36
900	1	2.01	1.674	.7	1.404	0.3559	4.59	0.00022	26.64
600	.300	1.566	1.419</						

TABLE IV. - THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(a) Percent fluorine in oxidant, O (100 percent oxygen)

Pressure ratio, P_o/P	Static pressure, P_s , lb/sq in. abs	Temperature, T_s , °K	Enthalpy, h_s , cal/g	Specific heat, c_p , cal/(g·°K)	Isentropic exponent, γ	Area ratio, a	Thrust coefficient, C_T , lb-sec/lb	Specific impulse, I_{sp} , sec
$r_s = 1.00$; percent fuel, 20.04; O/F, 5.980								
1.000	600.00	3497	2645.8	0.819	1.201	---	0.181	---
1.040	576.92	3474	2633.9	0.819	1.201	2.398	0.181	32.1
1.478	405.84	3275	2530.8	0.815	1.203	1.033	0.865	100.0
1.774	338.20	3175	2479.7	0.813	1.204	1.000	.679	120.2
2.218	270.56	3057	2419.3	0.811	1.205	1.031	.792	140.4
10.000	60.00	2355	2066.8	0.812	1.215	2.84	1.267	224.4
20.000	30.00	2081	1933.4	0.812	1.220	3.57	1.205	249.0
20.414	29.392	2073	1929.7	0.811	1.220	3.62	1.209	249.6
40.000	15.00	1834	1815.6	0.811	1.226	3.82	1.517	268.6
40.827	14.696	1827	1812.3	0.810	1.227	5.91	1.520	269.3
60.000	10.00	1700	1753.4	0.814	1.231	7.81	1.573	276.7
100.000	6.00	1544	1681.4	0.814	1.237	11.37	1.635	289.7
300.000	2.00	1245	1548.7	0.813	1.251	85.79	1.744	309.0
$r_s = 1.30$; percent fuel, 24.88; O/F, 5.069								
1.000	600.00	3444	3237.1	0.863	1.207	---	0.162	33.7
1.040	576.92	3421	3224.1	0.864	1.207	2.408	0.162	33.7
1.483	405.84	3219	3110.5	0.860	1.209	1.033	.567	105.0
1.778	337.52	3119	3054.6	0.858	1.210	1.000	.681	126.0
2.222	270.00	3000	2988.5	0.858	1.211	1.030	.794	147.1
10.000	60.00	2296	2605.1	0.833	1.222	2.23	1.266	234.5
20.000	30.00	2022	2460.4	0.832	1.228	3.54	1.204	266.0
20.414	29.392	2014	2455.6	0.831	1.228	3.59	1.207	266.6
40.000	15.00	1775	2333.2	0.809	1.235	5.76	1.500	280.5
40.827	14.696	1768	2329.7	0.808	1.235	6.84	1.517	291.0
60.000	10.00	1643	2266.2	0.801	1.240	7.71	1.570	290.7
100.000	6.00	1487	2188.9	0.801	1.246	11.19	1.631	302.0
300.000	2.00	1190	2047.1	0.805	1.263	25.21	1.738	321.8
$r_s = 1.40$; percent fuel, 25.88; O/F, 2.850								
1.000	600.00	3372	3419.6	0.878	1.210	---	0.182	33.9
1.040	576.92	3349	3406.4	0.877	1.210	2.405	0.182	33.9
1.483	404.48	3148	3290.7	0.873	1.213	1.032	.568	105.0
1.780	337.07	3049	3234.0	0.871	1.214	1.000	.682	127.1
2.225	269.66	2931	3167.0	0.868	1.215	1.030	.795	148.3
10.000	60.00	2235	2779.5	0.844	1.226	2.22	1.266	236.0
20.000	30.00	1964	2633.6	0.832	1.233	3.52	1.203	261.5
20.414	29.392	1956	2629.5	0.832	1.233	3.57	1.206	262.2
40.000	15.00	1720	2505.6	0.818	1.240	5.71	1.513	282.0
40.827	14.696	1713	2502.0	0.818	1.240	5.80	1.516	288.6
60.000	10.00	1589	2438.3	0.810	1.245	7.64	1.567	298.2
100.000	6.00	1435	2350.8	0.808	1.252	11.08	1.628	303.5
300.000	2.00	1144	2219.1	0.802	1.270	24.86	1.734	323.2
$r_s = 1.50$; percent fuel, 27.32; O/F, 2.680								
1.000	600.00	3272	3595.5	0.900	1.215	---	0.182	34.0
1.040	576.92	3249	3582.0	0.900	1.215	2.407	0.182	34.0
1.483	403.85	3050	3465.8	0.894	1.217	1.032	.570	106.5
1.783	336.54	2952	3408.0	0.882	1.218	1.030	.683	127.6
2.229	266.23	2836	3341.0	0.878	1.219	1.030	.797	148.6
10.000	60.00	2152	8953.1	0.854	1.232	2.21	1.265	236.4
20.000	30.00	1886	2807.5	0.841	1.239	3.49	1.202	261.8
20.414	29.392	1879	2803.5	0.840	1.239	3.54	1.205	262.5
40.000	15.00	1647	2680.1	0.826	1.247	5.66	1.511	282.2
40.827	14.696	1641	2676.6	0.825	1.247	5.75	1.514	288.8
60.000	10.00	1519	2613.3	0.817	1.252	7.56	1.565	292.3
100.000	6.00	1369	2536.5	0.805	1.260	10.94	1.625	303.5
300.000	2.00	1084	2396.7	0.802	1.279	24.43	1.729	323.0
$r_s = 1.60$; percent fuel, 28.82; O/F, 2.443								
1.000	600.00	3147	3765.0	0.900	1.220	---	0.182	34.0
1.040	576.92	3125	3751.7	0.900	1.220	2.411	0.182	34.0
1.483	403.10	2929	3634.5	0.904	1.228	1.032	.572	106.6
1.786	336.91	2833	3577.7	0.902	1.233	1.000	.685	127.7
2.233	268.73	2719	3510.8	0.898	1.235	1.030	.798	148.7
10.000	60.00	2052	3126.3	0.862	1.238	2.20	1.265	235.8
20.000	30.00	1793	2988.4	0.848	1.246	3.47	1.200	261.0
20.414	29.392	1785	2987.5	0.847	1.246	3.52	1.204	261.6
40.000	15.00	1560	2857.0	0.832	1.255	5.60	1.508	281.1
40.827	14.696	1554	2855.9	0.831	1.255	5.68	1.511	281.6
60.000	10.00	1436	2791.4	0.823	1.261	7.47	1.562	291.1
100.000	6.00	1290	2716.2	0.809	1.265	10.77	1.621	302.1
300.000	2.00	1015	2579.6	0.802	1.289	23.93	1.723	321.1
$r_s = 1.80$; percent fuel, 31.09; O/F, 2.216								
1.000	600.00	2855	4086.6	0.918	1.231	---	0.183	33.6
1.040	576.92	2834	4073.6	0.918	1.238	2.419	0.183	33.6
1.488	401.35	2646	3958.1	0.911	1.235	1.031	.576	105.7
1.784	334.46	2556	3903.0	0.908	1.236	1.000	.689	126.4
2.242	267.57	2449	3838.1	0.904	1.236	1.029	.802	147.0
10.000	60.00	1824	3469.2	0.874	1.254	2.17	1.264	231.8
20.000	30.00	1588	3332.8	0.857	1.264	3.40	1.207	256.8
20.414	29.392	1575	3328.4	0.857	1.264	3.45	1.200	256.8
40.000	15.00	1366	3213.7	0.840	1.275	5.46	1.503	275.6
40.827	14.696	1360	3210.4	0.839	1.275	5.54	1.505	276.1
60.000	10.00	1285	3152.1	0.829	1.281	7.25	1.555	285.2
100.000	6.00	1116	3081.9	0.816	1.291	10.40	1.612	295.7
300.000	2.00	865	2956.0	0.809	1.312	22.82	1.710	313.6

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TABLE IV. - Continued. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(b) Percent fluorine in oxidant by weight, 19.19

Pressure ratio, P_o/P	Static pressure, P , lb/sq in. abs	Tempera- ture, T , °K	Enthalpy, h , cal/g	Specific heat, c_p , cal/ (g)(°K)	Isentropic exponent, γ	Area ratio, ϵ	Thrust coeffi- cient, C_F	Specific impulse, I , lb-sec lb
$r, 1.20$; percent fuel, 21.10; O/F, 3.740								
1.000	600.00	3622	3017.6	0.521	1.224	---	0.183	34.3
1.040	576.92	3596	3004.1	0.521	1.224	2.414	0.183	34.3
1.490	402.55	3366	2884.6	0.517	1.226	1.032	0.573	107.6
1.789	335.46	3284	2827.1	0.515	1.228	1.000	0.686	128.8
2.235	268.37	3122	2759.2	0.512	1.229	1.030	0.799	149.9
10.000	60.00	2349	2370.5	0.492	1.241	2.19	1.265	237.3
20.000	30.00	2050	2225.3	0.481	1.247	3.46	1.400	262.6
20.414	29.392	2042	2221.3	0.481	1.248	3.50	1.403	263.8
40.000	15.00	1784	2098.7	0.469	1.255	5.58	1.507	282.8
40.827	14.696	1777	2095.2	0.469	1.256	5.66	1.510	283.3
60.000	10.00	1642	2052.4	0.462	1.261	7.44	1.561	292.8
100.000	6.00	1476	1956.5	0.452	1.268	10.74	1.620	303.9
300.000	2.00	1163	1818.8	0.429	1.286	23.90	1.722	323.0
$r, 1.40$; percent fuel, 23.78; O/F, 3.206								
1.000	600.00	3536	3359.8	0.548	1.227	---	0.183	34.9
1.040	576.92	3511	3345.1	0.548	1.227	2.416	0.183	34.9
1.492	402.09	3283	3220.8	0.543	1.230	1.032	0.575	109.7
1.791	335.07	3173	3151.1	0.541	1.231	1.000	0.687	131.3
2.238	268.06	3042	3090.7	0.538	1.232	1.030	0.800	152.8
10.000	60.00	2281	2668.9	0.516	1.245	2.18	1.264	241.5
20.000	30.00	1987	2539.0	0.504	1.252	3.44	1.399	267.1
20.414	29.392	1979	2554.9	0.504	1.252	3.49	1.402	267.8
40.000	15.00	1725	2408.7	0.491	1.261	5.55	1.506	287.6
40.827	14.696	1718	2405.1	0.490	1.261	5.63	1.509	288.1
60.000	10.00	1586	2340.6	0.483	1.266	7.38	1.559	297.7
100.000	6.00	1422	2262.7	0.472	1.274	10.64	1.617	308.9
300.000	2.00	1116	2121.8	0.447	1.293	23.58	1.718	328.1
$r, 1.50$; percent fuel, 25.05; O/F, 2.992								
1.000	600.00	3460	3521.4	0.560	1.230	---	0.183	35.1
1.040	576.92	3435	3507.2	0.560	1.230	2.418	0.183	35.1
1.494	401.70	3209	3381.4	0.555	1.232	1.031	0.576	110.4
1.792	334.75	3100	3321.2	0.553	1.234	1.000	0.688	132.0
2.240	267.80	2971	3250.3	0.549	1.235	1.030	0.801	153.6
10.000	60.00	2221	2846.2	0.526	1.248	2.18	1.264	242.4
20.000	30.00	1932	2695.7	0.514	1.256	3.42	1.398	268.0
20.414	29.392	1924	2691.6	0.513	1.256	3.47	1.401	268.7
40.000	15.00	1674	2565.1	0.500	1.265	5.51	1.505	288.5
40.827	14.696	1667	2561.5	0.499	1.265	5.59	1.507	289.0
60.000	10.00	1537	2496.9	0.491	1.271	7.34	1.557	298.6
100.000	6.00	1377	2419.1	0.480	1.279	10.56	1.615	309.7
300.000	2.00	1076	2278.6	0.455	1.299	23.32	1.715	328.8
$r, 1.60$; percent fuel, 26.28; O/F, 2.805								
1.000	600.00	3362	3678.2	0.571	1.233	---	0.183	35.1
1.040	576.92	3337	3664.1	0.571	1.233	2.420	0.183	35.1
1.495	401.21	3115	3537.5	0.566	1.236	1.031	0.577	110.7
1.795	334.34	3008	3477.2	0.563	1.237	1.000	0.689	132.3
2.243	267.47	2882	3406.3	0.560	1.239	1.029	0.802	153.8
10.000	60.00	2146	3002.8	0.536	1.253	2.17	1.264	242.4
20.000	30.00	1863	2852.9	0.522	1.261	3.41	1.397	268.0
20.414	29.392	1855	2848.8	0.522	1.261	3.45	1.401	268.6
40.000	15.00	1611	2723.1	0.507	1.270	5.48	1.503	288.3
40.827	14.696	1604	2719.5	0.507	1.271	5.55	1.506	288.8
60.000	10.00	1477	2655.5	0.498	1.277	7.28	1.555	298.3
100.000	6.00	1320	2578.4	0.487	1.285	10.45	1.613	309.4
300.000	2.00	1028	2439.7	0.461	1.306	23.00	1.711	328.3
$r, 1.80$; percent fuel, 28.62; O/F, 2.483								
1.000	600.00	3119	3977.0	0.591	1.242	---	0.184	34.9
1.040	576.92	3096	3963.0	0.590	1.242	2.426	0.184	34.9
1.500	399.98	2882	3837.2	0.585	1.245	1.031	0.580	110.3
1.800	333.31	2780	3777.8	0.582	1.246	1.000	0.692	131.7
2.250	266.65	2659	3708.1	0.578	1.248	1.029	0.805	153.0
10.000	60.00	1963	3314.2	0.550	1.264	2.15	1.263	240.2
20.000	30.00	1695	3168.6	0.535	1.274	3.36	1.395	265.2
20.414	29.392	1687	3164.6	0.535	1.274	3.41	1.398	265.9
40.000	15.00	1457	3043.2	0.519	1.285	5.38	1.499	285.1
40.827	14.696	1450	3039.8	0.519	1.285	5.46	1.502	285.6
60.000	10.00	1331	2978.2	0.509	1.292	7.13	1.550	294.8
100.000	6.00	1184	2904.4	0.497	1.301	10.20	1.607	305.5
300.000	2.00	912	2772.7	0.472	1.322	22.24	1.702	323.7

TABLE IV. - Continued. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(c) Percent fluorine in oxidant by weight, 37.25

Pressure ratio, P_o/P	Static pressure, P , lb/sq in. abs	Tempera- ture, T , °K	Enthalpy, h , cal/g	Specific heat, c_p , cal (g)°K	Isentropic exponent, γ	Area ratio, ϵ	Thrust coefficient, C_F	Specific impulse, I , lb-sec lb
r, 1.50; percent fuel, 20.36; O/F, 3.813								
1.000	600.00	3753	3145.8	0.505	1.247	2.429	0.184	35.7
1.040	576.92	3724	3131.2	0.505	1.247	2.429	0.184	35.7
1.502	399.38	3461	2999.1	0.501	1.249	1.031	.582	113.0
1.803	338.81	3337	2937.2	0.498	1.251	1.000	.694	134.7
2.254	266.25	3191	2864.4	0.496	1.253	1.029	.806	156.5
10.000	60.00	2349	2454.6	.476	1.266	2.14	1.263	245.3
20.000	30.00	2027	2303.2	.465	1.274	3.35	1.394	270.8
20.414	29.392	2018	2299.1	.464	1.274	3.40	1.398	271.4
40.000	15.00	1743	2172.8	.453	1.283	5.37	1.498	291.0
40.827	14.696	1735	2169.2	.452	1.284	5.44	1.501	291.5
60.000	10.00	1592	2105.2	.445	1.290	7.11	1.549	300.9
100.000	6.00	1418	2028.5	.435	1.298	10.18	1.606	311.8
300.000	2.00	1095	1891.1	.414	1.319	22.26	1.701	330.4
r, 1.50; percent fuel, 22.77; O/F, 3.391								
1.000	600.00	3650	3447.2	0.530	1.248	2.450	0.184	36.2
1.040	576.92	3621	3432.2	0.530	1.248	2.450	0.184	36.2
1.503	399.14	3364	3296.7	0.525	1.251	1.031	.582	114.5
1.804	338.61	3243	3233.2	0.523	1.253	1.000	.694	136.5
2.255	266.09	3100	3158.6	0.520	1.254	1.029	.806	158.5
10.000	60.00	2277	2739.4	.498	1.269	2.14	1.263	248.2
20.000	30.00	1963	2584.8	.486	1.277	3.34	1.394	273.9
20.414	29.392	1955	2580.5	.486	1.277	3.39	1.397	274.6
40.000	15.00	1686	2451.7	.473	1.287	5.34	1.498	294.3
40.827	14.696	1678	2448.1	.472	1.287	5.42	1.500	294.9
60.000	10.00	1539	2382.8	.465	1.293	7.08	1.548	304.3
100.000	6.00	1369	2304.7	.454	1.302	10.13	1.604	315.3
300.000	2.00	1053	2165.1	.431	1.323	22.07	1.699	334.0
r, 1.60; percent fuel, 23.93, O/F, 3.179								
1.000	600.00	3572	3591.2	0.541	1.250	2.431	0.184	36.3
1.040	576.92	3544	3576.1	0.541	1.250	2.431	0.184	36.3
1.504	398.88	3290	3439.6	0.536	1.253	1.031	.583	114.8
1.805	332.40	3171	3375.9	0.534	1.254	1.000	.695	136.9
2.256	265.92	3030	3301.0	0.531	1.256	1.029	.807	158.9
10.000	60.00	2222	2880.7	.508	1.271	2.14	1.263	248.6
20.000	30.00	1913	2725.8	.495	1.280	3.33	1.393	274.4
20.414	29.392	1905	2721.5	.495	1.280	3.38	1.397	275.1
40.000	15.00	1641	2592.9	.481	1.290	5.32	1.497	294.8
40.827	14.696	1633	2589.0	.481	1.290	5.40	1.499	295.3
60.000	10.00	1496	2523.9	.473	1.297	7.04	1.547	304.7
100.000	6.00	1329	2445.6	.462	1.306	10.07	1.603	315.7
300.000	2.00	1021	2306.7	.439	1.328	21.90	1.698	334.3
r, 1.70; percent fuel, 25.05; O/F, 2.992								
1.000	600.00	3479	3730.9	0.552	1.252	2.433	0.184	36.3
1.040	576.92	3451	3715.8	0.551	1.253	2.433	0.184	36.3
1.506	398.53	3202	3579.0	0.546	1.255	1.030	.584	115.0
1.807	332.11	3085	3515.3	0.544	1.257	1.000	.696	137.0
2.258	265.69	2947	3440.5	0.541	1.259	1.029	.808	159.0
10.000	60.00	2155	3021.3	.516	1.274	2.13	1.262	248.5
20.000	30.00	1853	2867.1	.503	1.284	3.32	1.393	274.2
20.414	29.392	1845	2862.9	.503	1.284	3.37	1.396	274.8
40.000	15.00	1586	2734.8	.489	1.294	5.30	1.496	294.4
40.827	14.696	1579	2731.2	.488	1.295	5.37	1.498	294.9
60.000	10.00	1446	2666.5	.480	1.301	7.00	1.546	304.3
100.000	6.00	1282	2589.1	.469	1.311	10.00	1.601	315.2
300.000	2.00	982	2451.5	.446	1.332	21.69	1.695	333.6
r, 1.90; percent fuel, 27.19; O/F, 2.677								
1.000	600.00	3258	3998.3	0.571	1.258	2.437	0.185	36.0
1.040	576.92	3231	3983.4	0.570	1.259	2.437	0.185	36.0
1.509	397.64	2992	3847.7	0.565	1.262	1.030	.586	114.5
1.811	331.37	2881	3784.9	0.562	1.264	1.000	.698	136.3
2.263	265.09	2750	3711.3	0.558	1.266	1.029	.809	158.0
10.000	60.00	1998	3300.8	.532	1.283	2.12	1.262	246.4
20.000	30.00	1711	3150.3	.517	1.293	3.29	1.391	271.6
20.414	29.392	1703	3146.2	.517	1.294	3.34	1.395	272.3
40.000	15.00	1459	3021.8	.501	1.305	5.23	1.493	291.5
40.827	14.696	1452	3018.3	.501	1.306	5.30	1.496	292.0
60.000	10.00	1325	2955.6	.492	1.313	6.90	1.543	301.2
100.000	6.00	1172	2880.9	.481	1.323	9.82	1.597	311.8
300.000	2.00	890	2748.8	.458	1.344	21.16	1.689	329.7

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TABLE IV. - Continued. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300

FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(d) Percent fluorine in oxidant by weight, 54.29

Pressure ratio, P_o/P	Static pressure, P_o , lb/sq in. abs	Tempera-ture, T , °K	Enthalpy, h , cal/g (g)(°K)	Specific heat, c_p , cal (g)(°K)	Isentropic exponent, γ	Area ratio, ϵ	Thrust coeffi-cient, C_F	Specific impulse, I_{sp} , lb-sec lb
$r, 1.30$; percent fuel, 16.26; O/F, 4.475								
1.000	600.00	3957	3100.6	0.476	1.271	-	-	-
1.040	576.92	3924	3084.9	0.475	1.271	2.444	0.185	36.9
1.515	396.05	3620	2941.1	0.471	1.274	1.030	.591	117.8
1.818	330.04	3481	2875.5	0.469	1.276	1.000	.702	139.9
2.272	264.03	3316	2798.7	0.467	1.278	1.028	.813	162.1
10.000	60.00	2388	2373.6	0.448	1.293	2.10	1.261	251.5
20.000	30.00	2037	2218.4	0.437	1.302	3.25	1.389	277.1
20.414	29.392	2028	2214.2	0.437	1.302	3.30	1.393	277.7
40.000	15.00	1731	2086.2	0.426	1.313	5.15	1.490	297.1
40.827	14.696	1723	2082.6	0.425	1.313	5.23	1.492	297.6
60.000	10.00	1571	2018.4	0.419	1.320	6.79	1.539	306.9
100.000	6.00	1386	1942.0	0.409	1.329	9.65	1.592	317.5
300.000	2.00	1049	1807.1	0.390	1.351	20.74	1.682	335.5
$r, 1.40$; percent fuel, 19.40; O/F, 4.156								
1.000	600.00	3917	3238.7	0.488	1.270	-	-	-
1.040	576.92	3885	3222.9	0.487	1.270	2.444	0.185	37.2
1.515	396.15	3585	3077.3	0.483	1.273	1.030	.590	118.5
1.817	330.13	3447	3010.9	0.481	1.275	1.000	.701	140.8
2.272	264.10	3285	2933.0	0.478	1.277	1.028	.813	163.1
10.000	60.00	2366	2502.1	0.459	1.292	2.10	1.261	253.2
20.000	30.00	2019	2344.7	0.448	1.301	3.25	1.389	278.9
20.414	29.392	2010	2340.5	0.448	1.302	3.30	1.393	279.6
40.000	15.00	1716	2210.7	0.436	1.312	5.16	1.490	299.1
40.827	14.696	1708	2207.1	0.436	1.313	5.23	1.493	299.6
60.000	10.00	1557	2141.9	0.429	1.319	6.80	1.539	308.9
100.000	6.00	1374	2064.4	0.419	1.329	9.66	1.592	319.7
300.000	2.00	1040	1927.6	0.400	1.351	20.76	1.683	337.8
$r, 1.50$; percent fuel, 20.50; O/F, 5.879								
1.000	600.00	3864	3373.1	0.499	1.270	-	-	-
1.040	576.92	3832	3357.1	0.499	1.270	2.444	0.185	37.3
1.515	396.17	3536	3210.2	0.495	1.273	1.030	.590	119.1
1.817	330.14	3400	3143.1	0.492	1.275	1.000	.701	141.5
2.272	264.11	3240	3064.5	0.490	1.277	1.028	.812	163.9
10.000	60.00	2334	2629.6	0.469	1.292	2.10	1.261	254.4
20.000	30.00	1992	2470.8	0.458	1.302	3.25	1.389	280.2
20.414	29.392	1982	2466.4	0.458	1.302	3.30	1.393	280.9
40.000	15.00	1693	2335.5	0.446	1.313	5.16	1.490	300.5
40.827	14.696	1684	2331.8	0.445	1.313	5.23	1.493	301.0
60.000	10.00	1536	2266.1	0.438	1.320	6.80	1.539	310.4
100.000	6.00	1355	2187.8	0.428	1.330	9.66	1.592	321.1
300.000	2.00	1025	2049.9	0.408	1.351	20.74	1.682	339.3
$r, 1.60$; percent fuel, 21.57; O/F, 5.836								
1.000	600.00	3798	3503.9	0.511	1.270	-	-	-
1.040	576.92	3766	3487.8	0.510	1.270	2.444	0.185	37.4
1.515	396.11	3475	3340.0	0.505	1.274	1.030	.590	119.4
1.817	330.09	3341	3272.6	0.503	1.275	1.000	.702	141.9
2.272	264.07	3184	3193.5	0.500	1.277	1.028	.813	164.3
10.000	60.00	2293	2756.4	0.479	1.293	2.10	1.261	255.0
20.000	30.00	1955	2596.8	0.467	1.303	3.25	1.389	280.9
20.414	29.392	1946	2592.5	0.467	1.303	3.30	1.393	281.6
40.000	15.00	1661	2461.0	0.454	1.314	5.15	1.490	301.2
40.827	14.696	1653	2457.3	0.454	1.314	5.22	1.492	301.8
60.000	10.00	1506	2391.3	0.447	1.321	6.78	1.539	311.1
100.000	6.00	1328	2312.8	0.436	1.331	9.64	1.592	321.9
300.000	2.00	1004	2174.5	0.416	1.353	20.68	1.682	340.1
$r, 1.80$; percent fuel, 23.65; O/F, 5.252								
1.000	600.00	3628	3755.1	0.531	1.272	-	-	-
1.040	576.92	3598	3739.0	0.531	1.273	2.446	0.185	37.4
1.516	395.76	3317	3590.9	0.525	1.276	1.030	.591	119.5
1.819	329.80	3189	3583.5	0.523	1.278	1.000	.702	142.0
2.274	263.84	3037	3444.6	0.520	1.280	1.028	.813	164.4
10.000	60.00	2181	3008.7	0.496	1.297	2.09	1.261	254.8
20.000	30.00	1857	2849.9	0.484	1.307	3.24	1.389	280.6
20.414	29.392	1848	2845.6	0.483	1.308	3.28	1.392	281.3
40.000	15.00	1574	2715.0	0.470	1.319	5.12	1.489	300.8
40.827	14.696	1567	2711.3	0.470	1.319	5.19	1.491	301.4
60.000	10.00	1426	2645.9	0.462	1.327	6.74	1.537	310.7
100.000	6.00	1256	2568.1	0.451	1.337	9.56	1.590	321.4
300.000	2.00	946	2431.4	0.431	1.359	20.46	1.679	339.4

TABLE IV. - Continued. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(e) Percent fluorine in oxidant by weight, 70.37

Pressure ratio, P_o/P	Static pressure, P , lb/sq in. abs	Temperature, T , °K	Enthalpy, h , cal/g	Specific heat, c_p , cal/(g)(°K)	Isentropic exponent, γ	Area ratio, ϵ	Thrust coefficient, C_F	Specific impulse, i , lb-sec/lb
$r, 1.40$; percent fuel, 17.22; O/F, 4.809								
1.000	600.00	4209	3178.8	0.458	1.294	-----	-----	-----
1.040	576.92	4171	3161.7	0.458	1.294	2.459	0.186	38.6
1.527	392.88	3821	3001.9	0.454	1.298	1.029	.599	124.1
1.833	327.40	3664	2930.8	0.452	1.300	1.000	.709	146.9
2.291	261.92	3480	2847.8	0.449	1.302	1.028	.819	169.7
10.000	60.00	2456	2396.3	0.431	1.319	2.06	1.260	260.9
20.000	30.00	2073	2233.2	0.421	1.329	3.16	1.385	286.8
20.414	29.392	2062	2228.8	0.421	1.329	3.20	1.388	287.5
40.000	15.00	1742	2095.8	0.410	1.340	4.97	1.482	307.0
40.827	14.696	1733	2092.1	0.410	1.341	5.04	1.485	307.5
60.000	10.00	1571	2025.9	0.403	1.348	6.51	1.529	316.7
100.000	6.00	1375	1947.6	0.395	1.358	9.19	1.580	327.3
300.000	2.00	1022	1811.4	0.378	1.381	19.45	1.665	344.9
$r, 1.50$; percent fuel, 18.22; O/F, 4.488								
1.000	600.00	4157	3299.0	0.469	1.293	-----	-----	-----
1.040	576.92	4120	3281.7	0.469	1.293	2.459	0.186	38.8
1.527	393.02	3775	3120.7	0.464	1.297	1.029	.599	124.6
1.832	327.52	3520	3049.0	0.462	1.299	1.000	.709	147.5
2.290	262.01	3438	2965.3	0.460	1.301	1.028	.819	170.4
10.000	60.00	2428	2509.5	0.441	1.318	2.06	1.260	262.1
20.000	30.00	2051	2344.8	0.431	1.328	3.17	1.385	288.2
20.414	29.392	2040	2340.3	0.430	1.328	3.21	1.388	288.8
40.000	15.00	1724	2205.9	0.419	1.340	4.97	1.482	308.4
40.827	14.696	1715	2202.2	0.419	1.340	5.04	1.485	308.9
60.000	10.00	1554	2135.3	0.412	1.347	6.52	1.530	318.2
100.000	6.00	1361	2056.2	0.404	1.358	9.20	1.581	328.8
300.000	2.00	1012	1918.5	0.386	1.380	19.48	1.666	346.6
$r, 1.60$; percent fuel, 19.20; O/F, 4.208								
1.000	600.00	4091	3416.3	0.480	1.292	-----	-----	-----
1.040	576.92	4055	3398.9	0.479	1.293	2.458	0.186	38.8
1.526	393.08	3716	3237.2	0.475	1.296	1.029	.599	124.8
1.832	327.57	3564	3165.1	0.473	1.298	1.000	.709	147.8
2.290	262.05	3386	3080.9	0.470	1.300	1.028	.819	170.8
10.000	60.00	2392	2622.7	0.451	1.317	2.06	1.260	262.8
20.000	30.00	2020	2457.0	0.440	1.328	3.17	1.385	288.9
20.414	29.392	2010	2452.5	0.439	1.328	3.21	1.388	289.6
40.000	15.00	1698	2317.4	0.428	1.340	4.97	1.482	309.2
40.827	14.696	1689	2313.6	0.428	1.340	5.04	1.485	309.8
60.000	10.00	1531	2246.4	0.421	1.348	6.52	1.530	319.1
100.000	6.00	1340	2166.9	0.412	1.358	9.20	1.581	329.7
300.000	2.00	996	2028.4	0.394	1.380	19.48	1.666	347.5
$r, 1.70$; percent fuel, 20.16; O/F, 3.960								
1.000	600.00	4014	3530.8	0.490	1.292	-----	-----	-----
1.040	576.92	3979	3513.4	0.489	1.293	2.458	0.186	38.9
1.526	393.07	3646	3351.4	0.485	1.296	1.029	.599	124.9
1.832	327.56	3497	3279.2	0.482	1.298	1.000	.709	148.0
2.290	262.05	3322	3194.9	0.480	1.300	1.028	.819	171.0
10.000	60.00	2346	2735.9	0.459	1.318	2.06	1.260	263.0
20.000	30.00	1981	2570.1	0.448	1.328	3.16	1.385	289.1
20.414	29.392	1971	2565.6	0.448	1.329	3.21	1.388	289.8
40.000	15.00	1665	2430.3	0.436	1.341	4.97	1.482	309.4
40.827	14.696	1656	2426.6	0.436	1.341	5.04	1.485	310.0
60.000	10.00	1501	2359.2	0.429	1.349	6.51	1.529	319.3
100.000	6.00	1313	2279.7	0.419	1.359	9.19	1.581	329.9
300.000	2.00	976	2141.2	0.402	1.381	19.45	1.666	347.7

TABLE IV. - Continued. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(f) Percent fluorine in oxidant by weight, 78.08

Pressure ratio, P_o/P	Static pressure, P , lb/sq in. abs	Tempera- ture, T , °K	Enthalpy, h , cal/g	Specific heat, c_p , cal (°K)	Isentropic exponent, γ	Area ratio, ϵ	Thrust coeffi- cient, C_F	Specific impulse, I , lb-sec lb
<i>r, 1.55; percent fuel, 17.55; O/F, 4.697</i>								
1.000	600.00	4333	3317.5	0.450	1.303	—	—	—
1.040	576.92	4293	3299.4	0.459	1.303	2.465	0.187	39.7
1.532	391.56	3922	3129.4	0.458	1.307	1.028	.602	127.9
1.838	326.50	3757	3054.6	0.450	1.309	1.000	.712	151.2
2.298	261.12	3564	2967.3	0.430	1.311	1.027	.822	174.6
10.000	60.00	2496	2495.3	0.433	1.328	2.04	1.259	267.5
20.000	30.00	2099	2355.4	0.423	1.339	3.13	1.383	293.8
20.414	29.392	2088	2320.8	0.422	1.339	3.17	1.387	294.5
40.000	15.00	1758	2182.8	0.412	1.351	4.90	1.479	314.2
40.827	14.696	1748	2179.0	0.411	1.351	4.97	1.482	314.7
60.000	10.00	1581	2110.6	0.408	1.359	6.41	1.526	324.1
100.000	6.00	1379	2029.8	0.396	1.369	9.02	1.576	334.7
300.000	2.00	1019	1889.9	0.380	1.392	18.99	1.659	352.4
<i>r, 1.60; percent fuel, 18.02; O/F, 4.551</i>								
1.000	600.00	4298	3372.4	0.455	1.303	—	—	—
1.040	576.92	4259	3354.3	0.454	1.303	2.465	0.187	39.7
1.532	391.72	3821	3184.0	0.450	1.307	1.028	.602	128.0
1.838	326.53	3726	3109.0	0.450	1.309	1.000	.712	151.4
2.298	261.15	3536	3021.5	0.435	1.311	1.027	.822	174.7
10.000	60.00	2477	2548.3	0.437	1.328	2.04	1.259	267.8
20.000	30.00	2083	2378.0	0.427	1.339	3.13	1.383	294.2
20.414	29.392	2073	2373.4	0.427	1.339	3.17	1.387	294.8
40.000	15.00	1744	2235.1	0.416	1.351	4.90	1.479	314.6
40.827	14.696	1735	2231.2	0.415	1.351	4.97	1.482	315.1
60.000	10.00	1569	2162.6	0.409	1.359	6.41	1.526	324.5
100.000	6.00	1369	2061.7	0.400	1.369	9.02	1.576	335.1
300.000	2.00	1011	1941.4	0.384	1.392	18.99	1.659	352.9
<i>r, 1.65; percent fuel, 18.46; O/F, 4.413</i>								
1.000	600.00	4228	3426.7	0.470	1.300	—	—	—
1.040	576.92	4190	3408.8	0.470	1.301	2.463	0.187	39.5
1.532	392.03	3831	3240.7	0.465	1.304	1.029	.601	127.8
1.837	326.69	3671	3165.5	0.463	1.306	1.000	.711	150.5
2.298	261.36	3483	3079.9	0.460	1.308	1.027	.821	173.7
10.000	60.00	2445	2610.7	0.442	1.326	2.05	1.259	266.5
20.000	30.00	2058	2441.7	0.431	1.336	3.14	1.384	292.8
20.414	29.392	2047	2437.2	0.431	1.337	3.18	1.387	293.4
40.000	15.00	1724	2299.8	0.420	1.349	4.92	1.480	313.1
40.827	14.696	1715	2295.9	0.420	1.349	4.98	1.483	313.7
60.000	10.00	1551	2227.7	0.413	1.357	6.43	1.527	323.0
100.000	6.00	1354	2147.5	0.404	1.367	9.06	1.577	333.7
300.000	2.00	1002	2007.7	0.387	1.389	19.09	1.661	351.4
<i>r, 1.68; percent fuel, 18.86; O/F, 5.003</i>								
1.000	600.00	4418	3232.1	0.450	1.305	—	—	—
1.040	576.92	4377	3213.9	0.449	1.306	2.467	0.187	39.7
1.532	391.36	3995	3043.1	0.445	1.310	1.028	.603	128.2
1.840	326.13	3826	2968.2	0.443	1.311	1.000	.713	151.5
2.300	260.91	3626	2880.7	0.441	1.314	1.027	.823	174.9
10.000	60.00	2537	2408.6	0.423	1.331	2.04	1.259	267.7
20.000	30.00	2151	2238.7	0.414	1.341	3.12	1.383	293.0
20.414	29.392	2140	2234.2	0.413	1.341	3.16	1.387	293.6
40.000	15.00	1783	2096.4	0.403	1.353	4.88	1.479	314.4
40.827	14.696	1774	2092.5	0.403	1.353	4.95	1.481	314.9
60.000	10.00	1603	2024.2	0.397	1.361	6.39	1.528	324.2
100.000	6.00	1398	1943.7	0.388	1.371	8.99	1.575	334.8
300.000	2.00	1031	1804.3	0.372	1.394	18.89	1.658	352.5
<i>r, 1.81; percent fuel, 16.86; O/F, 4.904</i>								
1.000	600.00	4402	3265.2	0.453	1.305	—	—	—
1.040	576.92	4362	3247.0	0.452	1.305	2.466	0.187	39.8
1.532	391.41	3981	3075.9	0.448	1.309	1.028	.603	128.3
1.840	326.17	3813	3000.7	0.446	1.311	1.000	.713	151.7
2.300	260.94	3616	2913.0	0.444	1.313	1.027	.823	175.1
10.000	60.00	2520	2439.6	0.426	1.330	2.04	1.259	268.0
20.000	30.00	2125	2269.3	0.416	1.341	3.12	1.382	294.0
20.414	29.392	2124	2264.7	0.415	1.341	3.16	1.386	294.6
40.000	15.00	1778	2120.5	0.406	1.353	4.89	1.479	315.0
40.827	14.696	1768	2120.7	0.405	1.353	4.95	1.481	315.5
60.000	10.00	1598	2054.2	0.399	1.361	6.39	1.528	324.6
100.000	6.00	1394	1973.4	0.391	1.371	8.99	1.575	335.3
300.000	2.00	1028	1833.6	0.375	1.394	18.90	1.658	352.9
<i>r, 1.85; percent fuel, 17.51; O/F, 4.777</i>								
1.000	600.00	4351	3309.0	0.457	1.305	—	—	—
1.040	576.92	4312	3290.9	0.457	1.303	2.465	0.187	39.6
1.532	391.67	3939	3121.3	0.458	1.307	1.028	.602	127.8
1.838	326.39	3773	3046.6	0.450	1.309	1.000	.712	151.1
2.298	261.11	3579	2959.4	0.448	1.311	1.027	.822	174.4
10.000	60.00	2507	2488.3	0.430	1.328	2.04	1.259	267.2
20.000	30.00	2108	2318.7	0.420	1.339	3.12	1.383	293.5
20.414	29.392	2097	2314.2	0.419	1.339	3.16	1.387	294.2
40.000	15.00	1765	2176.4	0.409	1.351	4.90	1.479	313.9
40.827	14.696	1755	2172.6	0.409	1.354	4.97	1.482	314.4
60.000	10.00	1587	2104.3	0.402	1.359	6.41	1.526	323.8
100.000	6.00	1385	2023.7	0.394	1.369	9.02	1.576	334.4
300.000	2.00	1023	1884.1	0.378	1.392	18.99	1.659	352.1

TABLE IV. - Continued. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(h) Percent fluorine in oxidant by weight, 80.15

Pressure ratio, P_o/P	Static pressure, P , lb/sq in. abs	Temperature, T , °K	Enthalpy, h , cal/g	Specific heat, c_p , cal/(g·°K)	Isentropic exponent, γ	Area ratio, a	Thrust coefficient, C_f	Specific impulse, I_{sp} , lb-sec/lb
<i>r</i> , 1.46; percent fuel, 16.40; O/F , 5.098								
1.000	600.00	4440	3207.7	0.447	1.306	—	—	—
1.040	576.92	4399	3169.5	0.446	1.307	2.467	0.187	39.7
1.535	391.88	4015	3018.6	0.442	1.310	1.028	0.603	126.3
1.840	386.08	3844	2953.6	0.440	1.312	1.000	0.713	151.5
2.300	260.84	3645	2856.2	0.436	1.314	1.027	0.823	174.9
10.000	60.00	2547	2584.3	0.421	1.331	8.04	1.259	267.7
20.000	30.00	2139	2314.6	0.411	1.342	3.12	1.383	294.0
20.414	29.398	2128	2310.6	0.411	1.342	3.16	1.386	294.6
40.000	15.00	1789	2072.4	0.401	1.354	4.88	1.479	314.3
40.827	14.696	1780	2068.6	0.400	1.354	4.94	1.481	314.8
60.000	10.00	1608	2000.4	0.394	1.362	6.38	1.525	324.1
100.000	6.00	1402	1920.0	0.386	1.372	8.97	1.575	334.7
300.000	2.00	1034	1780.9	0.370	1.395	18.85	1.656	352.4
<i>r</i> , 1.46; percent fuel, 16.59; O/F , 5.028								
1.000	600.00	4431	3229.8	0.449	1.306	—	—	—
1.040	576.92	4390	3211.6	0.446	1.306	2.467	0.187	39.8
1.535	391.89	4007	3040.4	0.444	1.310	1.028	0.603	126.4
1.840	386.08	3837	2965.3	0.442	1.312	1.000	0.713	151.7
2.300	260.86	3638	2877.6	0.440	1.314	1.027	0.823	175.1
10.000	60.00	2543	2404.7	0.428	1.331	8.04	1.259	267.9
20.000	30.00	2136	2234.7	0.413	1.341	3.12	1.383	294.3
20.414	29.398	2125	2230.1	0.413	1.342	3.16	1.386	294.9
40.000	15.00	1786	2092.1	0.402	1.354	4.88	1.479	314.6
40.827	14.696	1777	2068.3	0.402	1.354	4.95	1.481	315.2
60.000	10.00	1606	2019.9	0.396	1.361	6.39	1.525	324.5
100.000	6.00	1400	1939.3	0.388	1.372	8.98	1.575	335.1
300.000	2.00	1033	1799.8	0.378	1.394	18.87	1.656	352.7
<i>r</i> , 1.46; percent fuel, 16.77; O/F , 4.982								
1.000	600.00	4408	3251.8	0.451	1.305	—	—	—
1.040	576.92	4368	3233.7	0.450	1.305	2.466	0.187	39.7
1.535	391.40	3987	3063.0	0.446	1.309	1.028	0.603	126.2
1.840	386.17	3819	2988.1	0.444	1.311	1.000	0.713	151.5
2.300	260.94	3621	2900.7	0.442	1.313	1.027	0.823	174.8
10.000	60.00	2533	2428.6	0.424	1.330	8.04	1.259	267.6
20.000	30.00	2128	2258.9	0.415	1.341	3.12	1.383	293.9
20.414	29.398	2117	2254.9	0.414	1.341	3.16	1.386	294.5
40.000	15.00	1780	2116.4	0.404	1.353	4.89	1.479	314.6
40.827	14.696	1771	2112.6	0.404	1.353	4.95	1.481	314.8
60.000	10.00	1600	2044.3	0.398	1.361	6.39	1.525	324.1
100.000	6.00	1396	1963.8	0.389	1.371	8.99	1.575	334.8
300.000	2.00	1030	1824.3	0.373	1.394	18.91	1.656	352.4
<i>r</i> , 1.50; percent fuel, 16.77; O/F , 4.982								
1.000	600.00	4408	3251.8	0.451	1.305	—	—	—
1.040	576.92	4368	3233.7	0.450	1.305	2.466	0.187	39.7
1.535	391.40	3987	3063.0	0.446	1.309	1.028	0.603	126.2
1.840	386.17	3819	2988.1	0.444	1.311	1.000	0.713	151.5
2.300	260.94	3621	2900.7	0.442	1.313	1.027	0.823	174.8
10.000	60.00	2533	2428.6	0.424	1.330	8.04	1.259	267.6
20.000	30.00	2128	2258.9	0.415	1.341	3.12	1.383	293.9
20.414	29.398	2117	2254.9	0.414	1.341	3.16	1.386	294.5
40.000	15.00	1780	2116.4	0.404	1.353	4.89	1.479	314.6
40.827	14.696	1771	2112.6	0.404	1.353	4.95	1.481	314.8
60.000	10.00	1600	2044.3	0.398	1.361	6.39	1.525	324.1
100.000	6.00	1396	1963.8	0.389	1.371	8.99	1.575	334.8
300.000	2.00	1030	1824.3	0.373	1.394	18.91	1.656	352.4
<i>r</i> , 1.50; percent fuel, 16.77; O/F , 5.471								
1.000	600.00	4498	3113.3	0.436	1.309	—	—	—
1.040	576.92	4456	3095.2	0.435	1.309	2.469	0.187	39.6
1.535	390.95	4063	2924.2	0.431	1.313	1.028	0.604	126.1
1.840	385.74	3890	2880.5	0.429	1.315	1.000	0.714	151.5
2.300	260.59	3687	2763.3	0.427	1.317	1.027	0.824	174.5
10.000	60.00	2570	2825.3	0.410	1.334	8.03	1.259	266.8
20.000	30.00	2157	2127.9	0.401	1.345	3.11	1.383	299.9
20.414	29.398	2145	2122.7	0.401	1.345	3.15	1.386	299.5
40.000	15.00	1809	1990.1	0.392	1.355	4.89	1.475	312.1
40.827	14.696	1800	1986.3	0.391	1.356	4.95	1.478	312.2
60.000	10.00	1622	1917.8	0.385	1.364	6.37	1.522	322.5
100.000	6.00	1413	1836.5	0.377	1.375	8.95	1.573	333.3
300.000	2.00	1041	1698.8	0.368	1.397	18.99	1.656	350.8
<i>r</i> , 1.40; percent fuel, 16.84; O/F , 5.393								
1.000	600.00	4493	3135.6	0.438	1.308	—	—	—
1.040	576.92	4452	3117.4	0.437	1.309	2.469	0.187	39.7
1.535	390.95	4060	2946.6	0.433	1.313	1.028	0.604	126.2
1.840	385.74	3867	2881.6	0.431	1.315	1.000	0.714	151.5
2.300	260.59	3684	2764.6	0.429	1.317	1.027	0.823	174.6
10.000	60.00	2569	2315.0	0.418	1.334	8.04	1.259	267.2
20.000	30.00	2156	2146.3	0.403	1.344	3.11	1.383	293.4
20.414	29.398	2145	2141.7	0.403	1.344	3.15	1.386	294.1
40.000	15.00	1801	2005.0	0.393	1.356	4.89	1.478	313.6
40.827	14.696	1792	2001.2	0.393	1.357	4.95	1.480	314.2
60.000	10.00	1618	1933.5	0.387	1.364	6.35	1.524	323.4
100.000	6.00	1410	1883.7	0.379	1.375	8.93	1.574	334.0
300.000	2.00	1038	1715.8	0.363	1.397	18.76	1.656	351.5
<i>r</i> , 1.42; percent fuel, 15.85; O/F , 5.317								
1.000	600.00	4476	3167.7	0.440	1.308	—	—	—
1.040	576.92	4435	3139.6	0.440	1.308	2.468	0.187	39.7
1.535	391.06	4045	2969.1	0.438	1.312	1.028	0.604	126.1
1.841	385.88	3873	2882.4	0.435	1.314	1.000	0.714	151.4
2.301	260.71	3678	2807.3	0.431	1.316	1.027	0.823	174.6
10.000	60.00	2563	2337.8	0.414	1.333	8.04	1.259	267.1
20.000	30.00	2151	2169.0	0.405	1.343	3.11	1.383	293.3
20.414	29.398	2140	2164.5	0.405	1.344	3.15	1.386	294.0
40.000	15.00	1798	2027.7	0.395	1.355	4.87	1.478	313.6
40.827	14.696	1788	2023.9	0.395	1.356	4.93	1.481	314.1
60.000	10.00	1615	1956.1	0.389	1.363	6.36	1.524	323.3
100.000	6.00	1408	1876.3	0.380	1.374	8.95	1.574	333.9
300.000	2.00	1037	1738.8	0.365	1.396	18.80	1.657	351.4

TABLE IV. - Concluded. THEORETICAL ROCKET PERFORMANCE FOR PRESSURE RATIOS FROM 1 TO 300
FOR LIQUID METHANE WITH SEVERAL FLUORINE-OXYGEN MIXTURES

[Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 lb/sq in. abs.]

(j) Percent fluorine in oxidant by weight, 82.61

Pressure ratio, P_o/P	Static pressure, P , lb/sq in. abs	Tempera- ture, T , °K	Enthalpy, h , cal/g	Specific heat, c_p , cal (g)(°K)	Isentropic exponent, γ	Area ratio, ϵ	Thrust coeffi- cient, C_F	Specific impulse, I , lb-sec lb
r , 1.30; percent fuel, 14.53; O/F, 5.882								
1.000	600.00	4527	3019.9	0.425	1.312	-----	-----	-----
1.040	576.92	4485	3002.0	0.425	1.313	2.471	0.187	39.4
1.537	390.44	4085	2832.9	0.420	1.317	1.028	.606	127.5
1.844	325.37	3910	2759.2	0.419	1.319	1.000	.715	150.6
2.305	260.29	3704	2673.4	0.416	1.321	1.027	.824	173.6
10.000	60.00	2576	2212.0	0.400	1.338	2.03	1.259	265.1
20.000	30.00	2158	2046.5	0.392	1.348	3.10	1.382	291.0
20.414	29.392	2147	2042.0	0.391	1.348	3.14	1.385	291.7
40.000	15.00	1800	1908.1	0.382	1.360	4.84	1.477	311.0
40.827	14.696	1791	1904.4	0.381	1.361	4.90	1.479	311.5
60.000	10.00	1616	1838.1	0.376	1.368	6.31	1.523	320.7
100.000	6.00	1406	1760.2	0.368	1.379	8.87	1.572	331.1
300.000	2.00	1033	1625.6	0.353	1.401	18.58	1.654	348.3
r , 1.333; percent fuel, 14.85; O/F, 5.735								
1.000	600.00	4528	3057.2	0.429	1.311	-----	-----	-----
1.040	576.92	4486	3039.2	0.428	1.312	2.470	0.187	39.6
1.536	390.57	4087	2869.2	0.424	1.316	1.028	.605	127.9
1.843	325.47	3911	2795.0	0.422	1.318	1.000	.715	151.0
2.304	260.38	3706	2708.6	0.420	1.320	1.027	.824	174.2
10.000	60.00	2579	2243.8	0.404	1.337	2.03	1.259	266.0
20.000	30.00	2162	2077.0	0.395	1.347	3.10	1.382	292.0
20.414	29.392	2150	2072.5	0.395	1.347	3.14	1.385	292.7
40.000	15.00	1804	1937.5	0.385	1.359	4.84	1.477	312.1
40.827	14.696	1794	1933.8	0.385	1.360	4.91	1.480	312.7
60.000	10.00	1620	1867.0	0.379	1.367	6.32	1.523	321.8
100.000	6.00	1410	1788.3	0.371	1.378	8.89	1.572	332.3
300.000	2.00	1036	1652.6	0.356	1.400	18.63	1.654	349.6
r , 1.40; percent fuel, 15.48; O/F, 5.462								
1.000	600.00	4480	3131.0	0.436	1.307	-----	-----	-----
1.040	576.92	4438	3113.1	0.436	1.307	2.467	0.187	39.5
1.534	391.16	4049	2944.3	0.431	1.311	1.028	.604	127.4
1.841	325.97	3877	2870.3	0.430	1.313	1.000	.713	150.6
2.301	260.77	3676	2784.1	0.427	1.315	1.027	.823	173.7
10.000	60.00	2567	2318.9	0.411	1.332	2.04	1.259	265.8
20.000	30.00	2156	2151.6	0.402	1.342	3.12	1.383	291.9
20.414	29.392	2144	2147.1	0.401	1.343	3.16	1.386	292.6
40.000	15.00	1802	2011.5	0.391	1.354	4.87	1.478	312.1
40.827	14.696	1793	2007.7	0.391	1.355	4.94	1.481	312.6
60.000	10.00	1620	1940.5	0.385	1.362	6.37	1.525	321.9
100.000	6.00	1412	1861.3	0.377	1.373	8.96	1.574	332.4
300.000	2.00	1041	1724.3	0.362	1.395	18.83	1.657	349.9
r , 1.50; percent fuel, 16.40; O/F, 5.098								
1.000	600.00	4395	3239.7	0.448	1.300	-----	-----	-----
1.040	576.92	4356	3221.9	0.448	1.300	2.463	0.187	39.3
1.530	392.08	3982	3055.7	0.443	1.304	1.029	.601	126.5
1.836	326.74	3816	2982.2	0.441	1.306	1.000	.711	149.7
2.295	261.39	3622	2896.5	0.439	1.308	1.027	.821	172.8
10.000	60.00	2543	2432.0	0.421	1.325	2.05	1.259	265.1
20.000	30.00	2142	2264.6	0.412	1.335	3.14	1.384	291.3
20.414	29.392	2131	2260.1	0.412	1.335	3.18	1.387	291.9
40.000	15.00	1796	2124.0	0.401	1.347	4.92	1.480	311.6
40.827	14.696	1786	2120.2	0.401	1.347	4.99	1.483	312.1
60.000	10.00	1616	2052.5	0.395	1.354	6.44	1.527	321.4
100.000	6.00	1412	1972.7	0.387	1.365	9.08	1.577	332.0
300.000	2.00	1046	1834.1	0.371	1.387	19.16	1.662	349.7

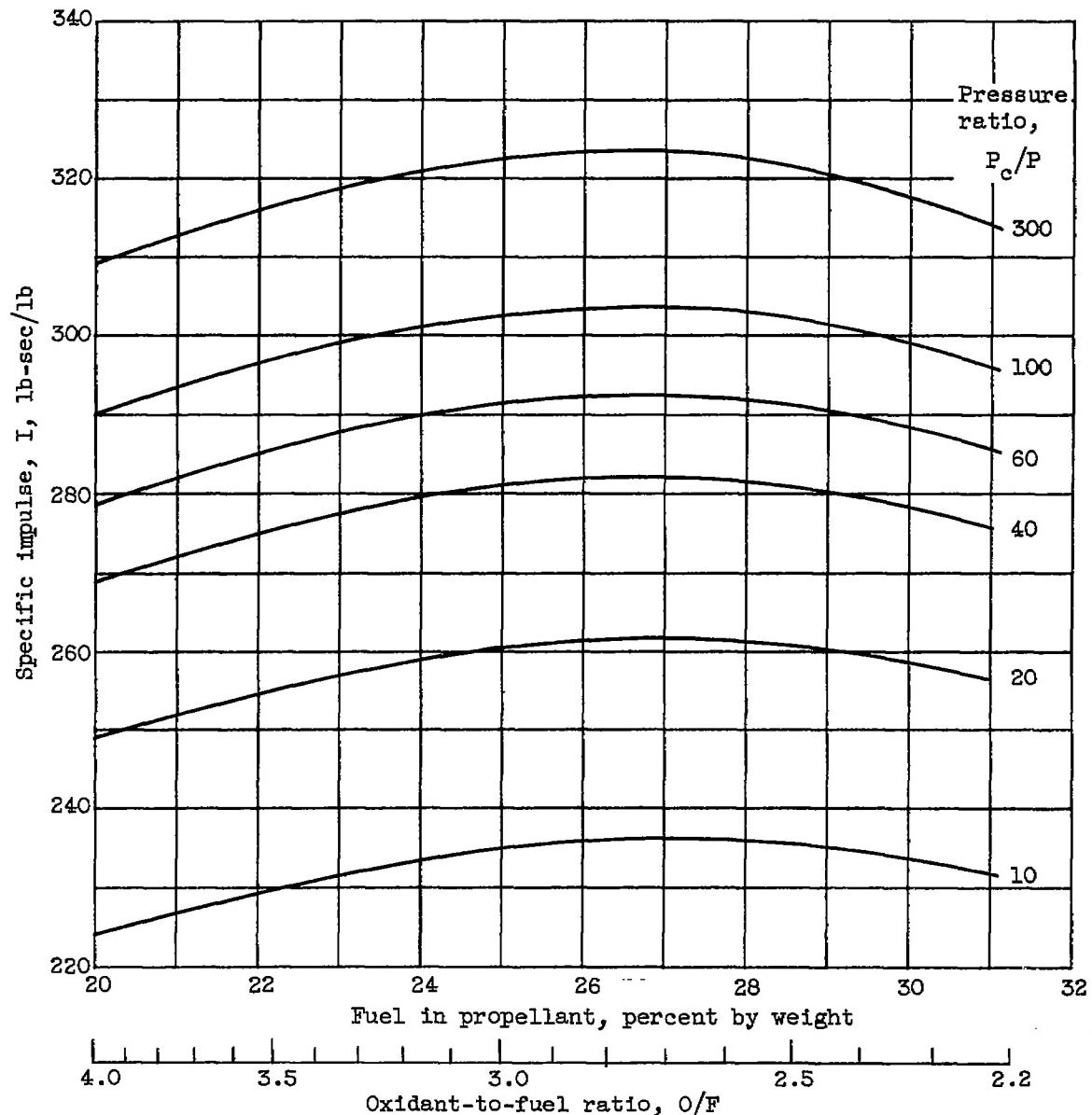
TABLE V. - EQUILIBRIUM COMPOSITION IN COMBUSTION CHAMBER FOR LIQUID METHANE WITH SEVERAL MIXTURES OF FLUORINE AND OXYGEN

Equiva- lence ratio, $\frac{r}{2}$ $\frac{(C)}{2} + \frac{(H)}{4}$	Fuel, percent by weight	Oxidant- to-fuel weight ratio, O/F	Equilibrium composition (mole fraction ^a)																
			C	CF	OF ₂	OF ₃	C ₂ F ₂	CO	CO ₂	F	F ₂	H	H ₂	HF	H ₂ O	O	O ₂	OH	
Percent fluorine in oxidant, 0 (100 percent oxygen)																			
1.00	80.04	5.990						0.15840	0.14751			0.02123	0.03398		0.46668	0.02138	0.07074	0.08027	
1.50	24.58	5.069						0.21085	0.10377			0.02780	0.11914		0.47275	0.00747	0.01135	0.04580	
1.40	25.98	5.850						0.21163	0.08879			0.02648	0.15085		0.46075	0.00395	0.00482	0.03270	
1.50	27.32	5.660						0.24966	0.07514			0.02292	0.18712		0.44122	0.00174	0.00158	0.02041	
1.60	28.82	5.493						0.26451	0.06355			0.01799	0.22588		0.41587	0.00065	0.00048	0.01141	
1.80	31.09	2.218						0.26452	0.04892			0.00849	0.30191		0.55536	0.00006	0.00003	0.00269	
Percent fluorine in oxidant by weight, 19.19																			
1.40	21.10	5.740						0.18558	0.06841	0.00154		0.05490	0.08425	0.18468	0.35161	0.01786	0.02688	0.08484	
1.40	25.78	5.208						0.22241	0.06792	0.00072		0.05680	0.13366	0.15009	0.33333	0.00749	0.00714	0.04074	
1.50	25.06	2.992						0.22827	0.05818	0.00048		0.05410	0.16475	0.14588	0.32607	0.00406	0.00308	0.02878	
1.60	26.28	2.805						0.25190	0.04948	0.00029		0.02970	0.18900	0.13670	0.31122	0.00182	0.00115	0.01865	
1.80	28.68	2.493						0.27257	0.03589	0.00008		0.01821	0.27038	0.12450	0.27190	0.00030	0.00012	0.00618	
Percent fluorine in oxidant by weight, 37.25																			
1.50	20.35	5.913						0.19628	0.06387	0.00354		0.04756	0.09144	0.30880	0.20844	0.01874	0.01634	0.08482	
1.50	22.77	5.591						0.22685	0.04103	0.00195		0.04784	0.14104	0.25588	0.21148	0.00775	0.00443	0.03427	
1.60	23.93	5.179						0.25877	0.05058	0.00132		0.04464	0.17091	0.27282	0.20568	0.00431	0.00199	0.02480	
1.70	25.06	2.992						0.28334	0.02874	0.00084		0.03951	0.20304	0.26183	0.19821	0.00216	0.00081	0.01851	
1.90	27.19	2.677						0.26603	0.02130	0.00029		0.02649	0.26902	0.24188	0.18846	0.00043	0.00010	0.00620	
Percent fluorine in oxidant by weight, 54.29																			
1.50	18.38	4.475						0.19147	0.06170	0.01100		0.06088	0.08984	0.44378	0.09860	0.02700	0.01459	0.04815	
1.40	18.40	4.156						0.20575	0.02795	0.00841		0.08430	0.09968	0.45268	0.10456	0.01902	0.00643	0.04112	
1.50	20.60	5.879						0.21612	0.02418	0.00624		0.06529	0.11264	0.41918	0.10709	0.01282	0.00458	0.03523	
1.60	21.57	5.858						0.22556	0.02053	0.00447		0.05386	0.15862	0.40567	0.10613	0.00782	0.00223	0.02631	
1.80	25.63	3.252						0.24337	0.01411	0.00005		0.04140	0.19751	0.37840	0.08458	0.00223	0.00041	0.01225	
Percent fluorine in oxidant by weight, 70.37																			
1.40	17.22	4.809						0.19456	0.01018	0.02982		0.08194	0.05458	0.65515	0.02473	0.02197	0.00362	0.02525	
1.50	18.22	4.488						0.20398	0.00826	0.02211		0.08769	0.07558	0.54398	0.02577	0.01414	0.00160	0.01878	
1.60	18.20	4.208						0.21271	0.00638	0.01635		0.08992	0.09579	0.53159	0.02475	0.00822	0.00061	0.01581	
1.70	20.16	3.960						0.22076	0.00436	0.01134		0.08656	0.12104	0.51848	0.06141	0.00422	0.00023	0.00601	
Percent fluorine in oxidant by weight, 78.08																			
1.50	17.55	4.887						0.20269	0.00068	0.04108		0.10280	0.05844	0.58875	0.00171	0.00216	0.00002	0.00197	
1.60	18.02	4.551	0.00011	0.00006				0.20643	0.00002	0.04940		0.10516	0.06818	0.58486	0.00006	0.00006			
1.65	18.48	4.415	0.00188	0.00154	0.00003			0.00157	0.20444		0.02712	0.10215	0.07875	0.58170					
Percent fluorine in oxidant by weight, 78.57																			
1.48	18.88	5.003	0.00001	0.00001				0.19577	0.00038	0.06005		0.09580	0.04187	0.80818	0.00071	0.00188	0.00001	0.00114	
1.51	18.84	4.904	0.00018	0.00012				0.00001	0.19799	0.00008	0.04942		0.10108	0.04844	0.88807	0.00004	0.00009		0.00006
1.55	17.31	4.777	0.00178	0.00141	0.00004			0.00103	0.19648	0.00008	0.04568		0.10087	0.05351	0.88918	0.00001			
Percent fluorine in oxidant by weight, 80.15																			
1.48	18.40	5.098	0.00001	0.00002				0.19373	0.00028	0.06874		0.09625	0.05776	0.60268	0.00047	0.00130	0.00001	0.00082	
1.48	16.59	5.028	0.00009	0.00008				0.19266	0.00004	0.06305		0.09845	0.04054	0.69215	0.00007	0.00017		0.00011	
1.50	16.77	4.932	0.00101	0.00065	0.00005			0.00029	0.18473	0.00005	0.05785		0.09875	0.04357	0.60286	0.00001	0.00001		0.00001
Percent fluorine in oxidant by weight, 81.46																			
1.38	15.45	5.471	0.00001	0.00001				0.18560	0.00029	0.09328		0.08635	0.02626	0.80710	0.00055	0.00172	0.00001	0.00082	
1.40	15.84	5.393	0.00007	0.00007				0.18747	0.00008	0.08877		0.08835	0.02758	0.80727	0.00007	0.00032		0.00014	
1.42	15.83	5.317	0.00059	0.00068	0.00003			0.00025	0.18721	0.00008	0.08870		0.08258	0.02652	0.80691	0.00001	0.00002		0.00001
Percent fluorine in oxidant by weight, 82.81																			
1.30	14.53	5.882	0.00001	0.00001				0.17758	0.00041	0.12375	0.00001	0.07130	0.01628	0.80854	0.00053	0.00277	0.00002	0.00103	
1.335	14.88	5.735	0.00114	0.00116	0.00001			0.00001	1.8043	0.00003	0.11498		0.07703	0.01898	0.80603	0.00003	0.00119		0.00008
1.40	15.48	5.488	0.00258	0.00253	0.00010	0.00001		0.00198	0.17829	0.00102	0.08504		0.08504	0.02814	0.81350	0.00001	0.00001		
1.50	16.40	5.098	0.00484	0.00397	0.00013	0.00001		0.00875	0.17478	0.00181	0.09078		0.08075	0.03611	0.81944				

^aMole fractions were computed for all 19 substances considered in this report but were omitted if less than 5×10^{-6} .

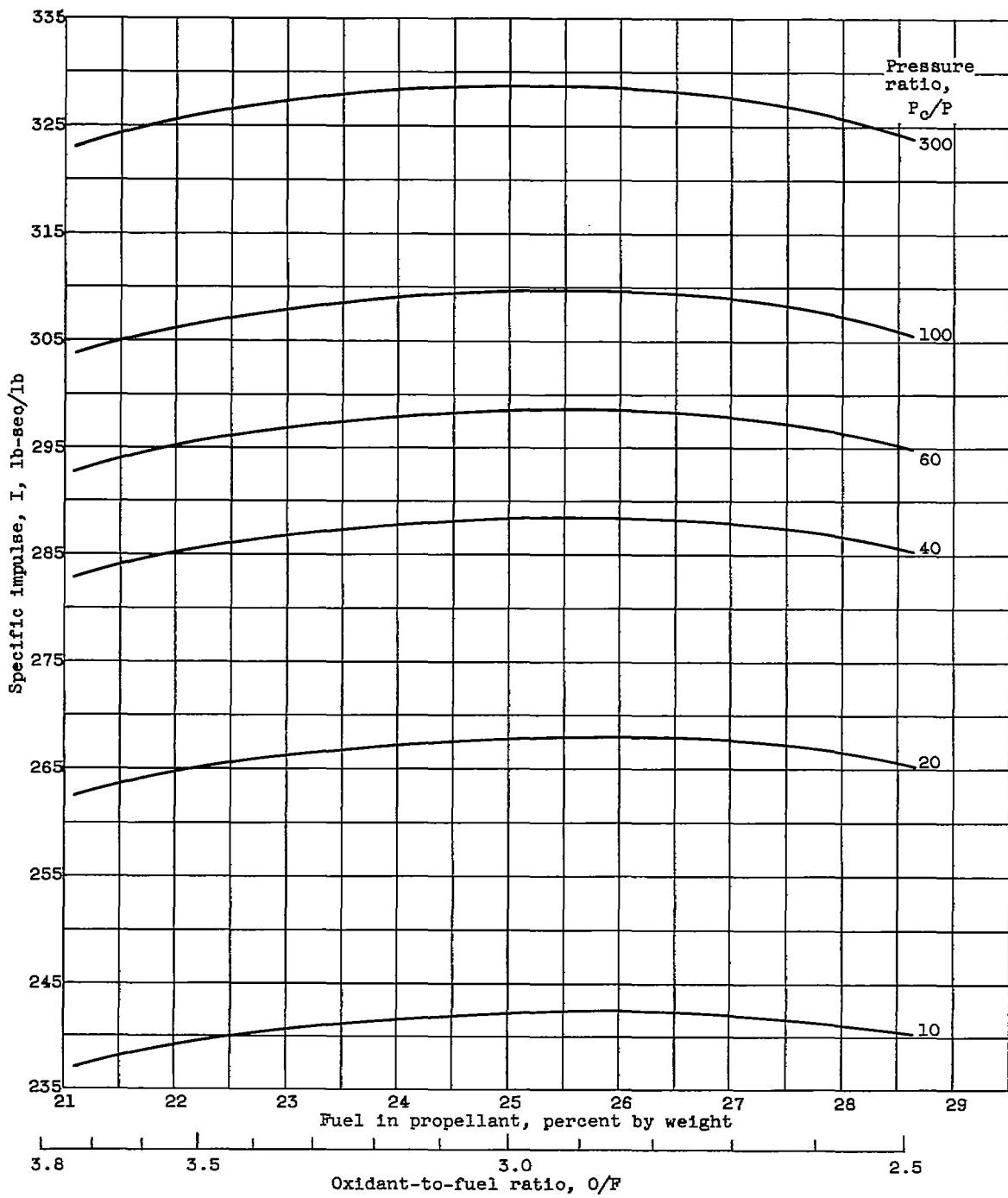
TABLE VI. - THEORETICAL ROCKET PERFORMANCE FOR EXPANSION TO EXIT
PRESSURE OF 1 ATMOSPHERE FOR LIQUID METHANE WITH SEVERAL
MIXTURES OF FLUORINE AND OXYGEN

Equivalence ratio, $\frac{r}{\frac{4(C) + (H)}{2(O) + (F)}}$	Fuel, percent by weight	Oxidant-to-fuel weight ratio, O/F	Combustion temperature, T_c , °K	Exit temperature, T_e , °K	Characteristic velocity, c^* , ft/sec	Area ratio, ϵ	Thrust coefficient, C_F	Specific impulse, I, lb-sec/lb
Percent fluorine in oxidant, 0 (100 percent oxygen)								
1.00	20.04	3.990	3497	1827	5700	5.91	1.520	269.3
1.30	24.58	3.069	3444	1768	5959	5.84	1.517	281.0
1.40	25.98	2.850	3372	1713	5998	5.80	1.516	282.6
1.50	27.32	2.660	3272	1641	6011	5.75	1.514	282.8
1.60	28.62	2.493	3147	1554	5996	5.68	1.511	281.6
1.80	31.09	2.216	2855	1360	5901	5.54	1.505	276.1
Percent fluorine in oxidant by weight, 19.19								
1.20	21.10	3.740	3622	1777	6036	5.66	1.510	283.3
1.40	23.78	3.206	3536	1718	6145	5.63	1.509	288.1
1.50	25.05	2.992	3460	1667	6169	5.59	1.507	289.0
1.60	26.28	2.805	3362	1604	6172	5.55	1.506	288.8
1.80	28.62	2.493	3119	1450	6118	5.46	1.502	285.6
Percent fluorine in oxidant by weight, 37.25								
1.30	20.35	3.913	3753	1735	6248	5.44	1.501	291.5
1.50	22.77	3.391	3650	1678	6324	5.42	1.500	294.9
1.60	25.93	3.179	3572	1633	6336	5.40	1.499	295.3
1.70	25.05	2.992	3479	1579	6333	5.37	1.498	294.9
1.90	27.19	2.677	3258	1452	6282	5.30	1.496	292.0
Percent fluorine in oxidant by weight, 54.29								
1.30	18.26	4.475	3957	1723	6416	5.23	1.492	297.6
1.40	19.40	4.156	3917	1708	6459	5.23	1.493	299.6
1.50	20.50	3.879	3864	1684	6489	5.23	1.493	301.0
1.60	21.57	3.636	3798	1653	6506	5.22	1.492	301.8
1.80	23.63	3.232	3628	1567	6503	5.19	1.491	301.4
Percent fluorine in oxidant by weight, 70.37								
1.40	17.22	4.809	4209	1733	6664	5.04	1.485	307.5
1.50	18.22	4.488	4157	1715	6694	5.04	1.485	308.9
1.60	19.20	4.208	4091	1689	6711	5.04	1.485	309.8
1.70	20.16	3.960	4014	1656	6717	5.04	1.485	310.0
Percent fluorine in oxidant by weight, 78.08								
1.55	17.55	4.697	4333	1748	6833	4.97	1.482	314.7
1.60	18.02	4.551	4298	1735	6841	4.97	1.482	315.1
1.65	18.48	4.413	4228	1715	6807	4.98	1.483	313.7
Percent fluorine in oxidant by weight, 79.67								
1.48	16.66	5.003	4418	1774	6840	4.95	1.481	314.9
1.51	16.94	4.904	4402	1768	6848	4.95	1.481	315.3
1.55	17.31	4.777	4351	1755	6827	4.97	1.482	314.4
Percent fluorine in oxidant by weight, 80.15								
1.46	16.40	5.098	4440	1780	6839	4.94	1.481	314.8
1.48	16.59	5.029	4431	1777	6846	4.95	1.481	315.2
1.50	16.77	4.962	4408	1771	6838	4.95	1.481	314.8
Percent fluorine in oxidant by weight, 81.46								
1.38	15.45	5.471	4498	1803	6817	4.96	1.479	313.5
1.40	15.64	5.393	4493	1792	6828	4.93	1.480	314.2
1.42	15.83	5.317	4476	1788	6825	4.93	1.481	314.1
Percent fluorine in oxidant by weight, 82.61								
1.30	14.53	5.882	4527	1791	6776	4.90	1.479	311.5
1.333	14.85	5.735	4528	1794	6799	4.91	1.480	312.7
1.40	15.48	5.462	4480	1793	6793	4.94	1.481	312.6
1.50	16.40	5.098	4395	1786	6772	4.99	1.483	312.1



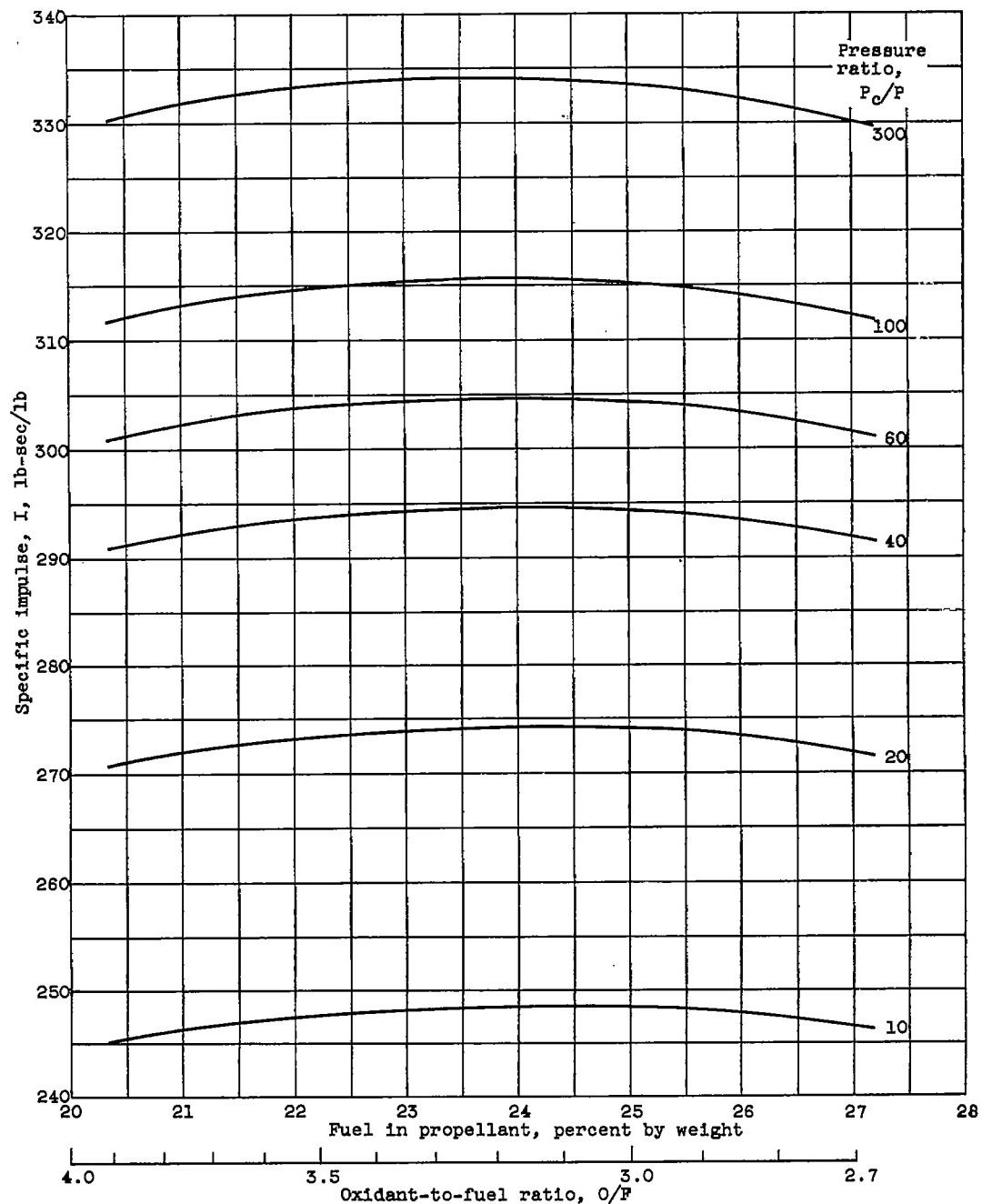
(a) Percent fluorine in oxidant by weight, O (100 percent oxygen).

Figure 1. - Theoretical specific impulse of liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



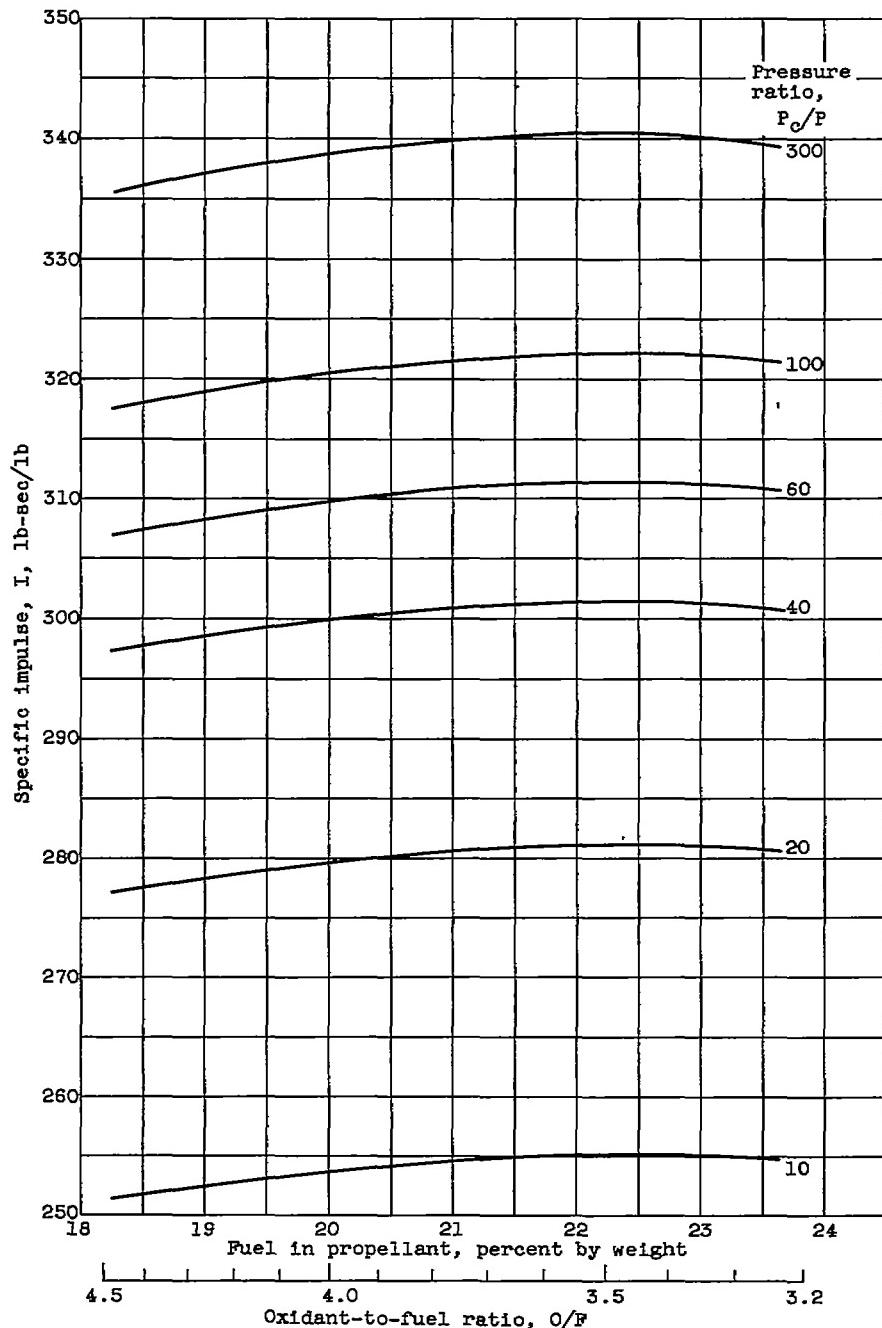
(b) Percent fluorine in oxidant by weight, 19.19.

Figure 1. - Continued. Theoretical specific impulse of liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



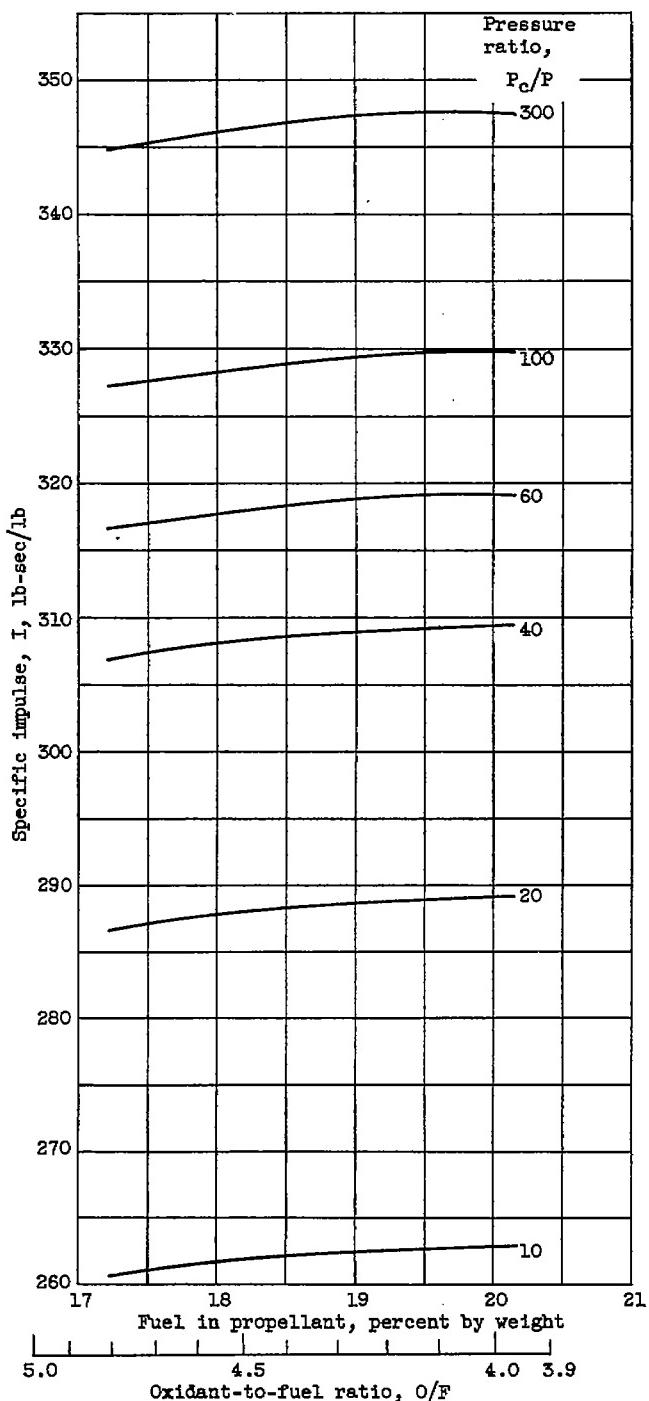
(c) Percent fluorine in oxidant, 37.25.

Figure 1. - Continued. Theoretical specific impulse of liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



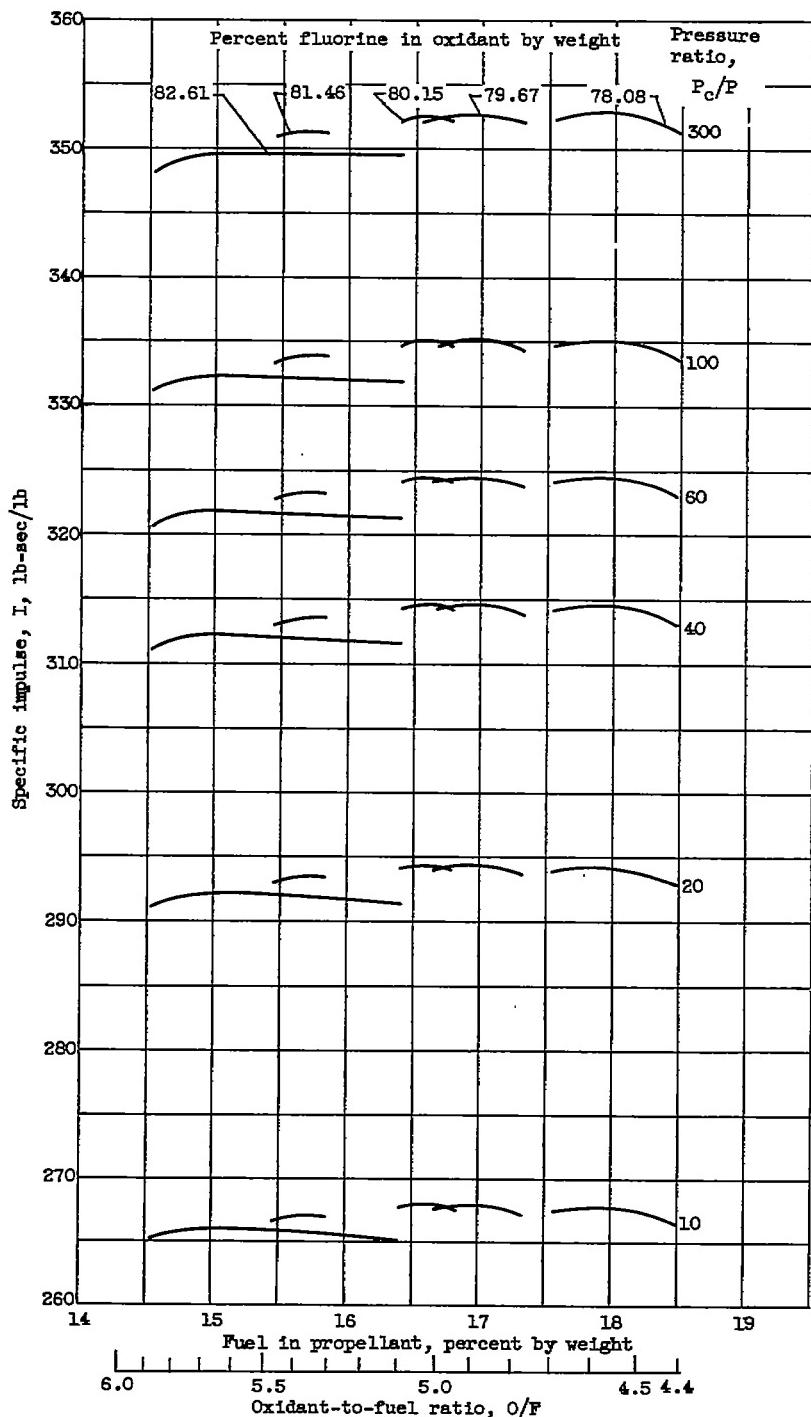
(d) Percent fluorine in oxidant by weight, 54.29.

Figure 1. - Continued. Theoretical specific impulse of liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



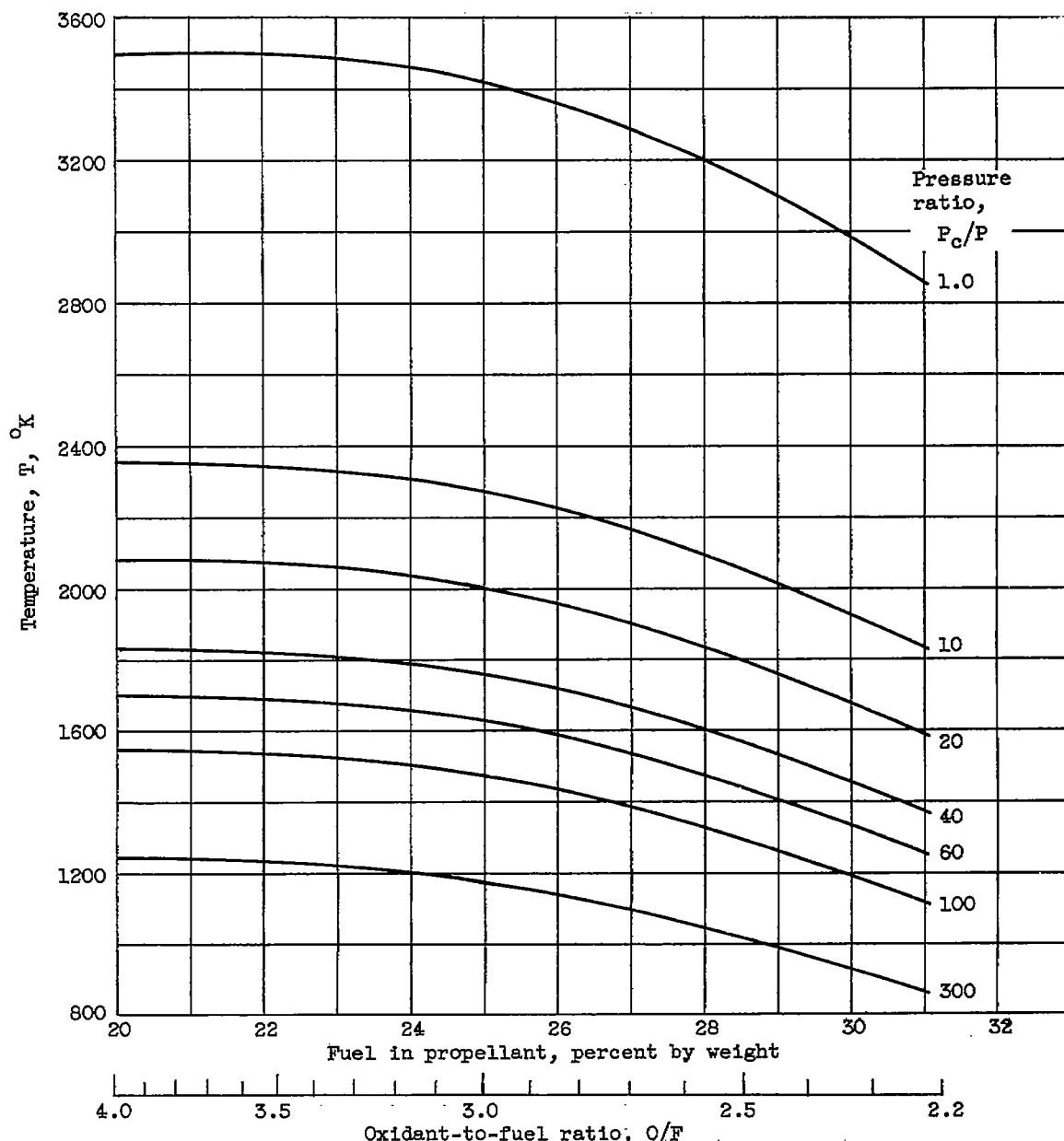
(e) Percent fluorine in oxidant by weight, 70.37.

Figure 1. - Continued. Theoretical specific impulse of liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



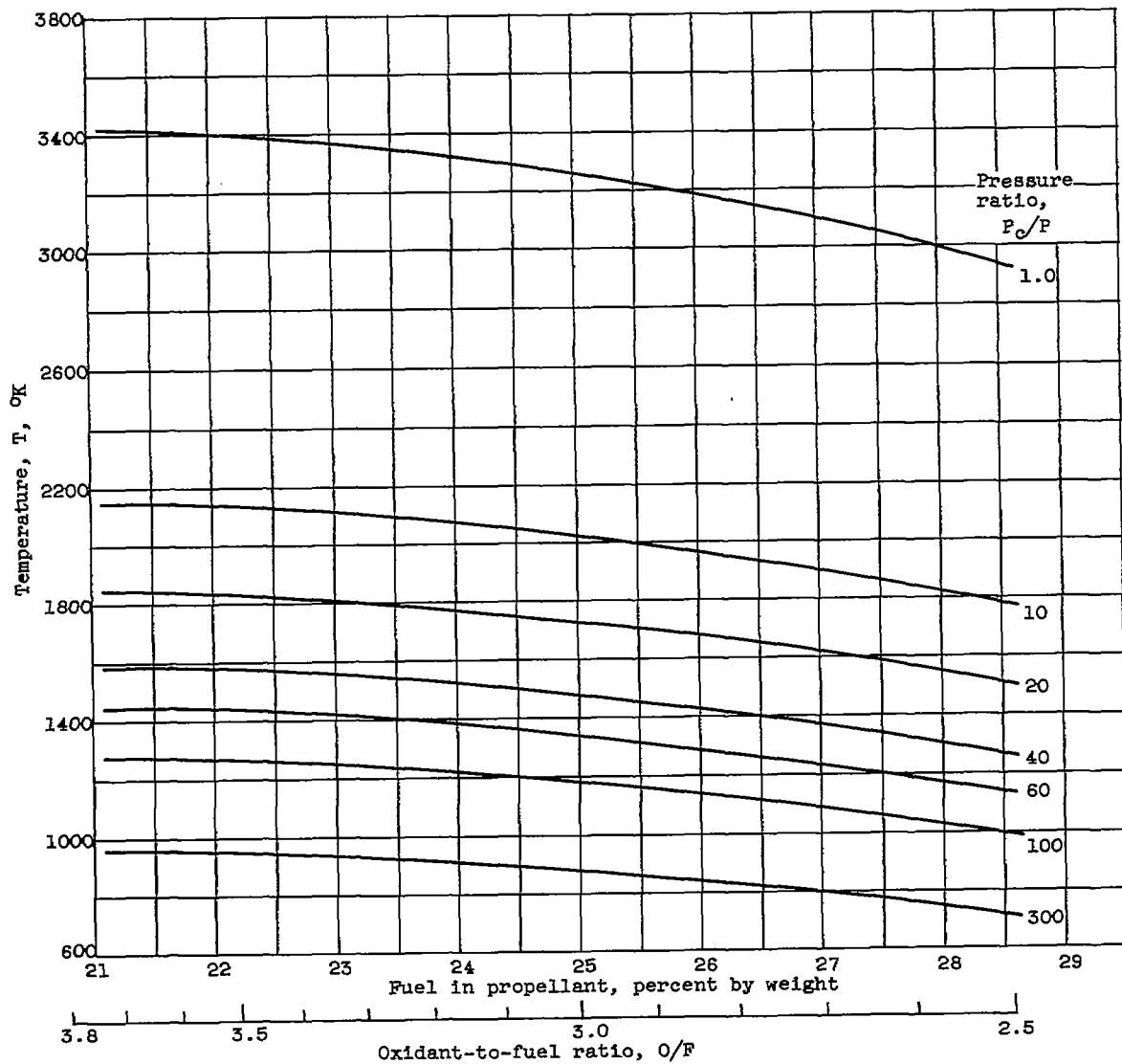
(f) Percent fluorine in oxidant by weight, 78.08 to 82.61.

Figure 1. - Concluded. Theoretical specific impulse of liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratios indicated.



(a) Percent fluorine in oxidant by weight, 0 (100 percent oxygen).

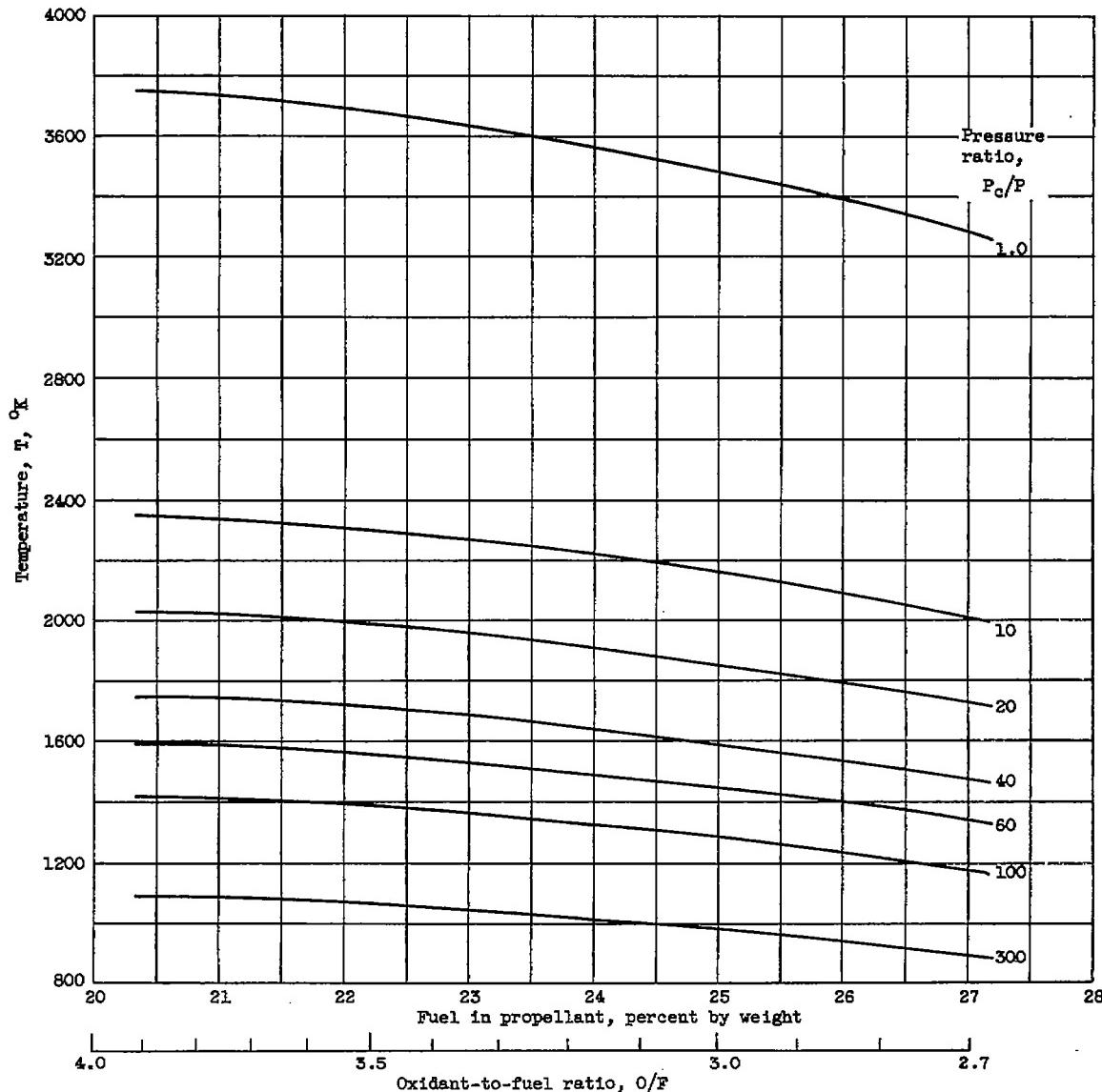
Figure 2. - Theoretical combustion-chamber temperature and nozzle-exit temperature for liquid methane and several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.

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(b) Percent fluorine in oxidant by weight, 19.19.

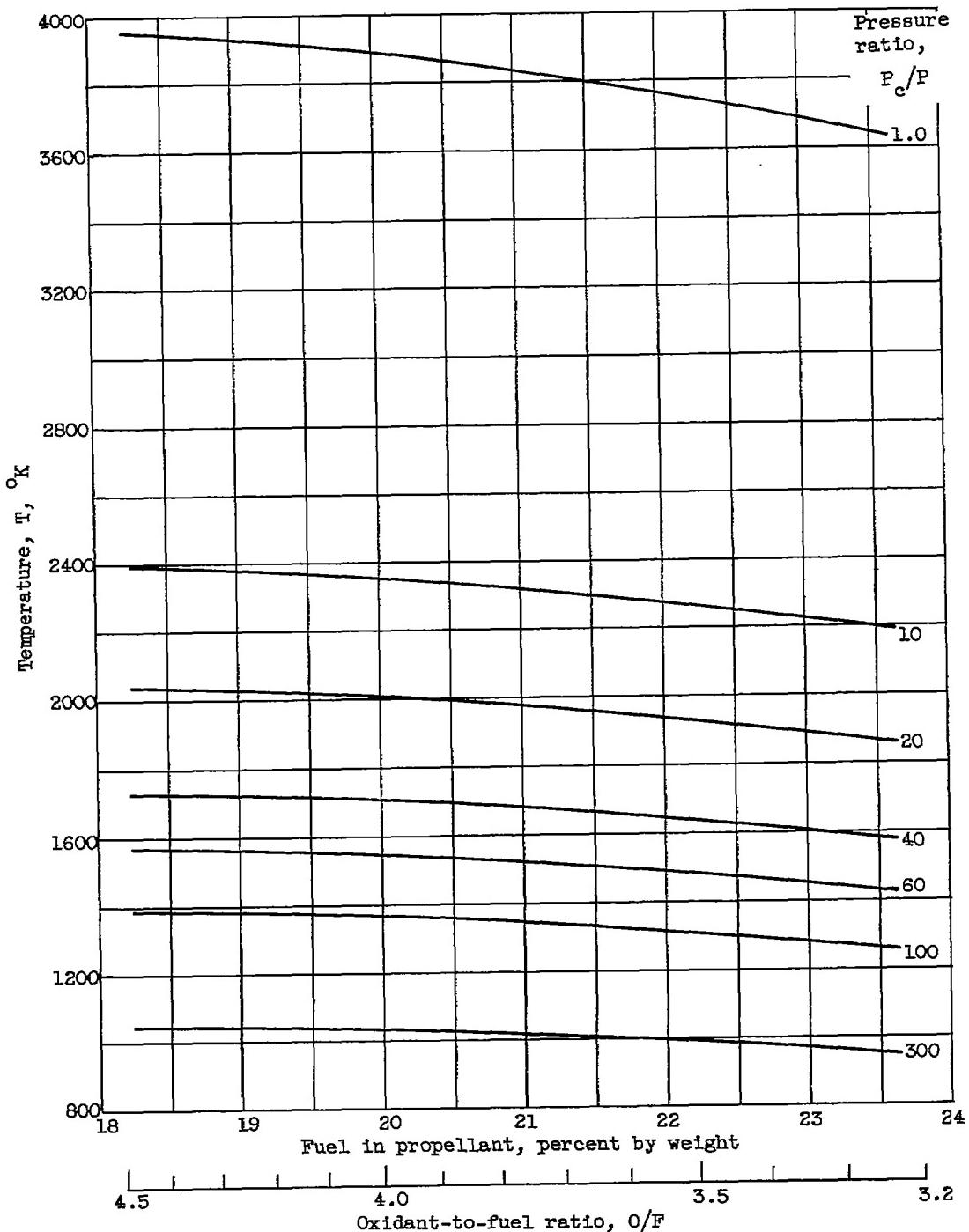
Figure 2. - Continued. Theoretical combustion-chamber temperature and nozzle-exit temperature for liquid methane and several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.

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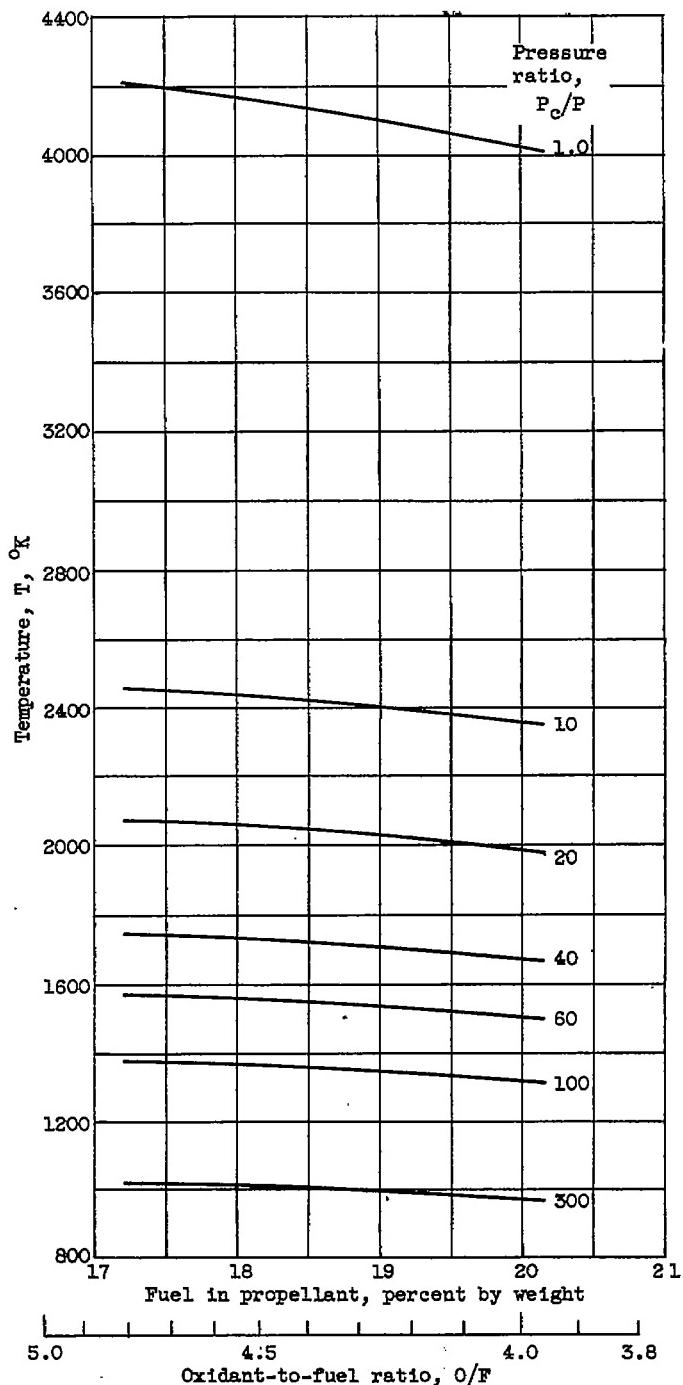
(c) Percent fluorine in oxidant by weight, 37.25.

Figure 2. - Continued. Theoretical combustion-chamber temperature and nozzle-exit temperature for liquid methane and several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



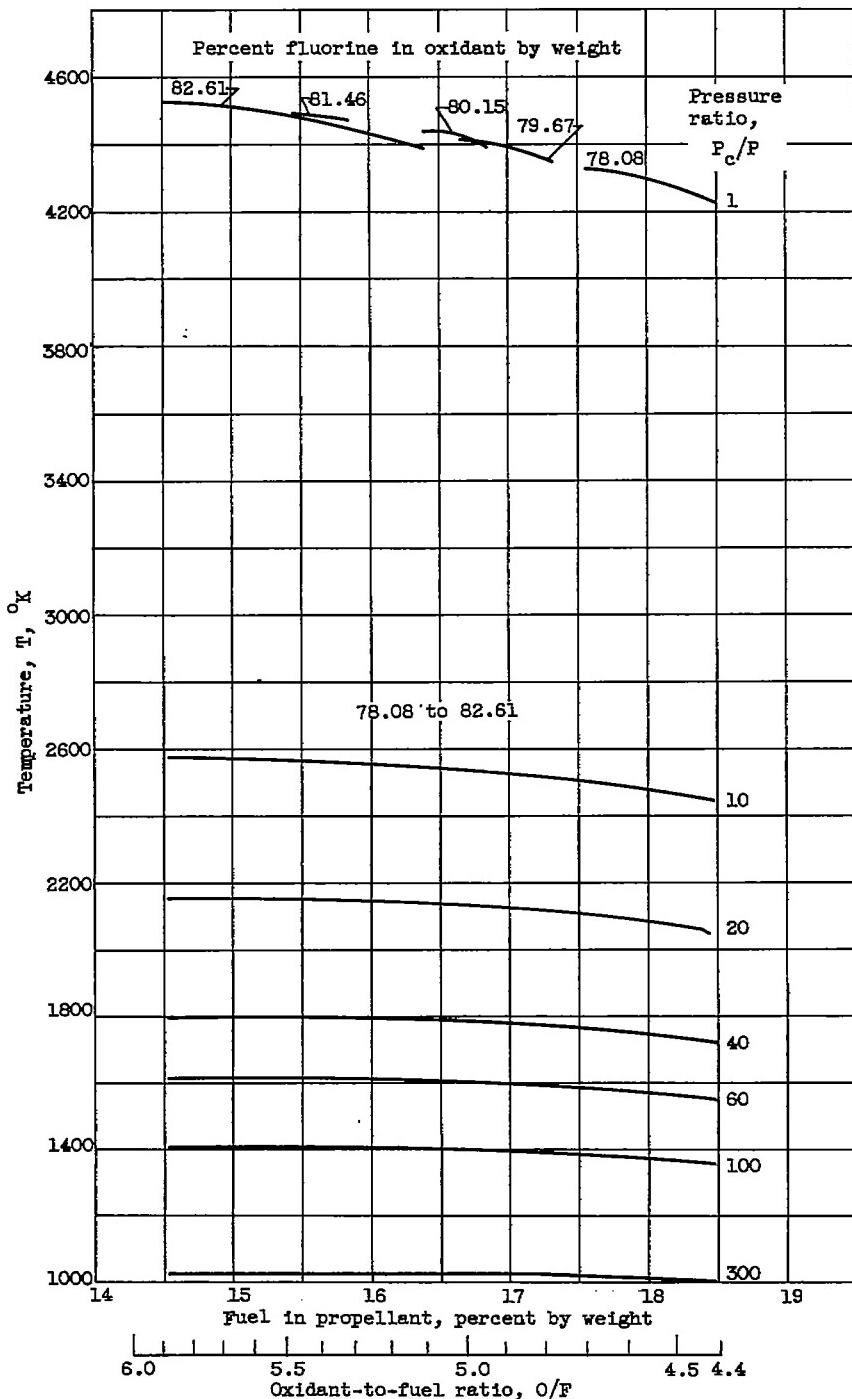
(d) Percent fluorine in oxidant by weight, 54.29.

Figure 2. - Continued. Theoretical combustion-chamber temperature and nozzle-exit temperature for liquid methane and several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



(e) Percent fluorine in oxidant by weight, 70.37.

Figure 2. - Continued. Theoretical combustion-chamber temperature and nozzle-exit temperature for liquid methane and several fluorine-oxygen mixtures. From composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.



(f) Percent fluorine in oxidant by weight, 78.08 to 82.61.

Figure 2. - Concluded. Theoretical combustion-chamber temperature and nozzle-exit temperature for liquid methane and several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.

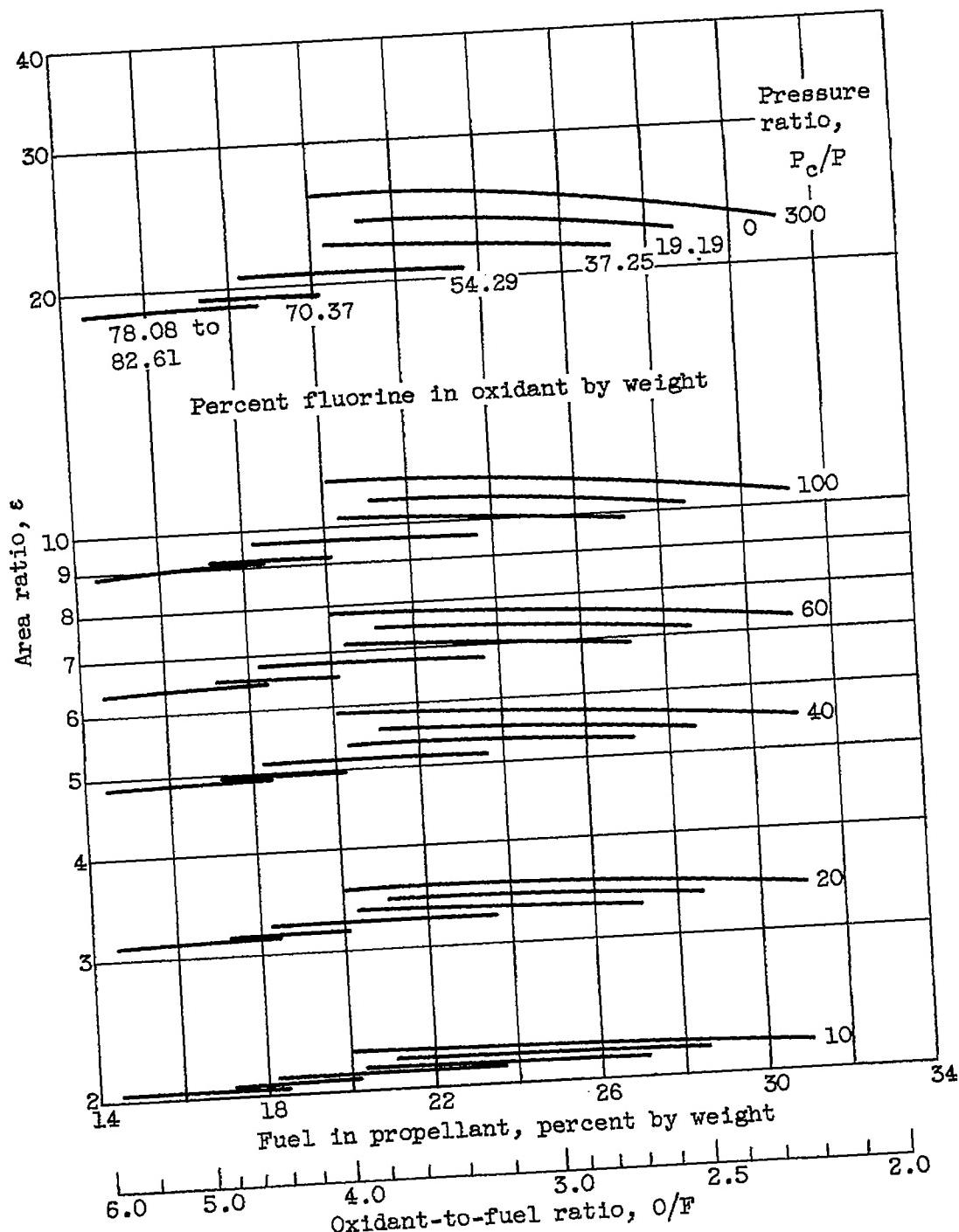


Figure 3. - Theoretical ratio of nozzle area to throat area for liquid methane with several fluorine-oxygen mixtures. Frozen composition during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to pressure ratio indicated.

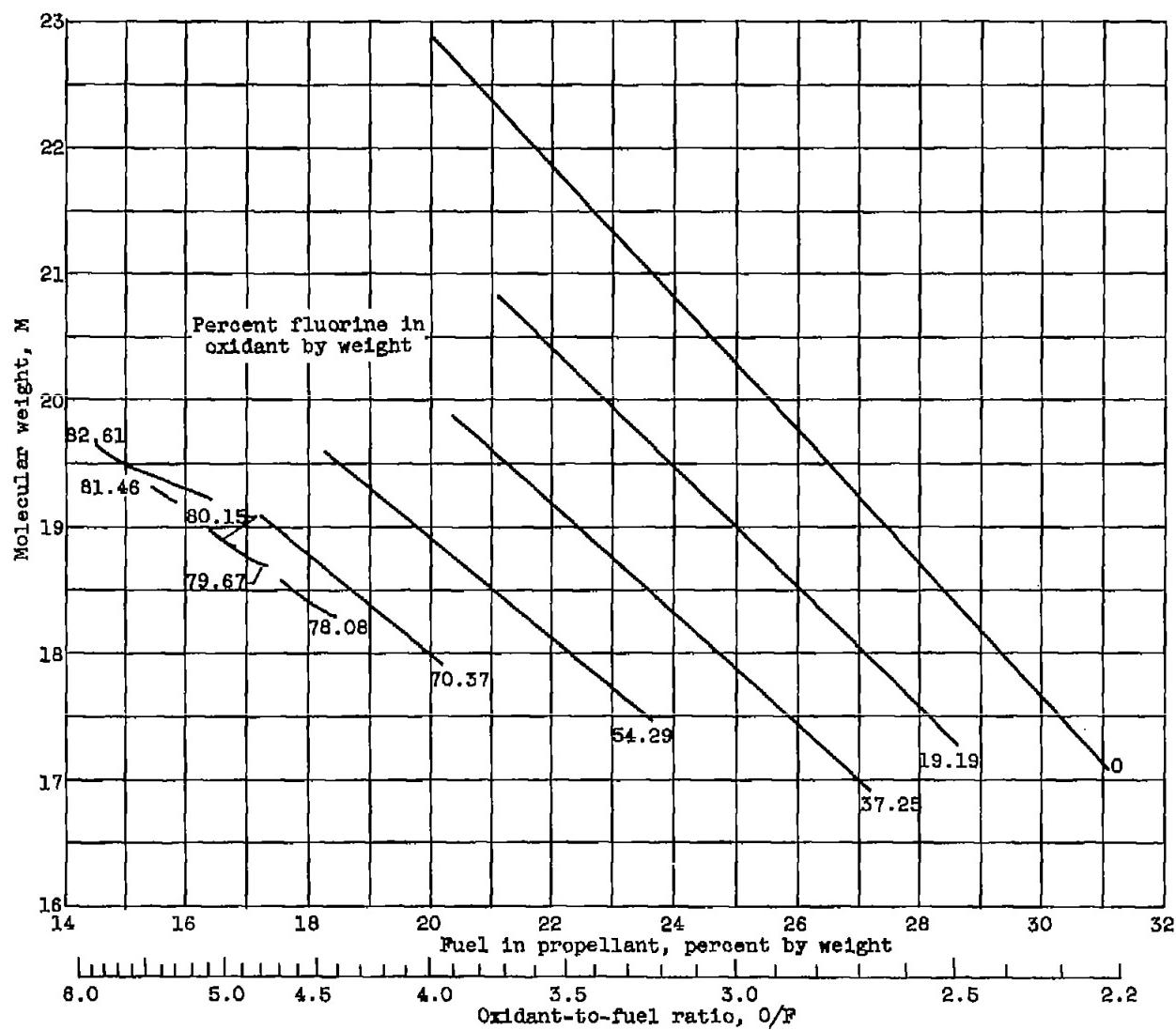


Figure 4. - Theoretical combustion-chamber molecular weight for liquid methane with several fluorine-oxygen mixtures. Combustion-chamber pressure, 600 pounds per square inch absolute.

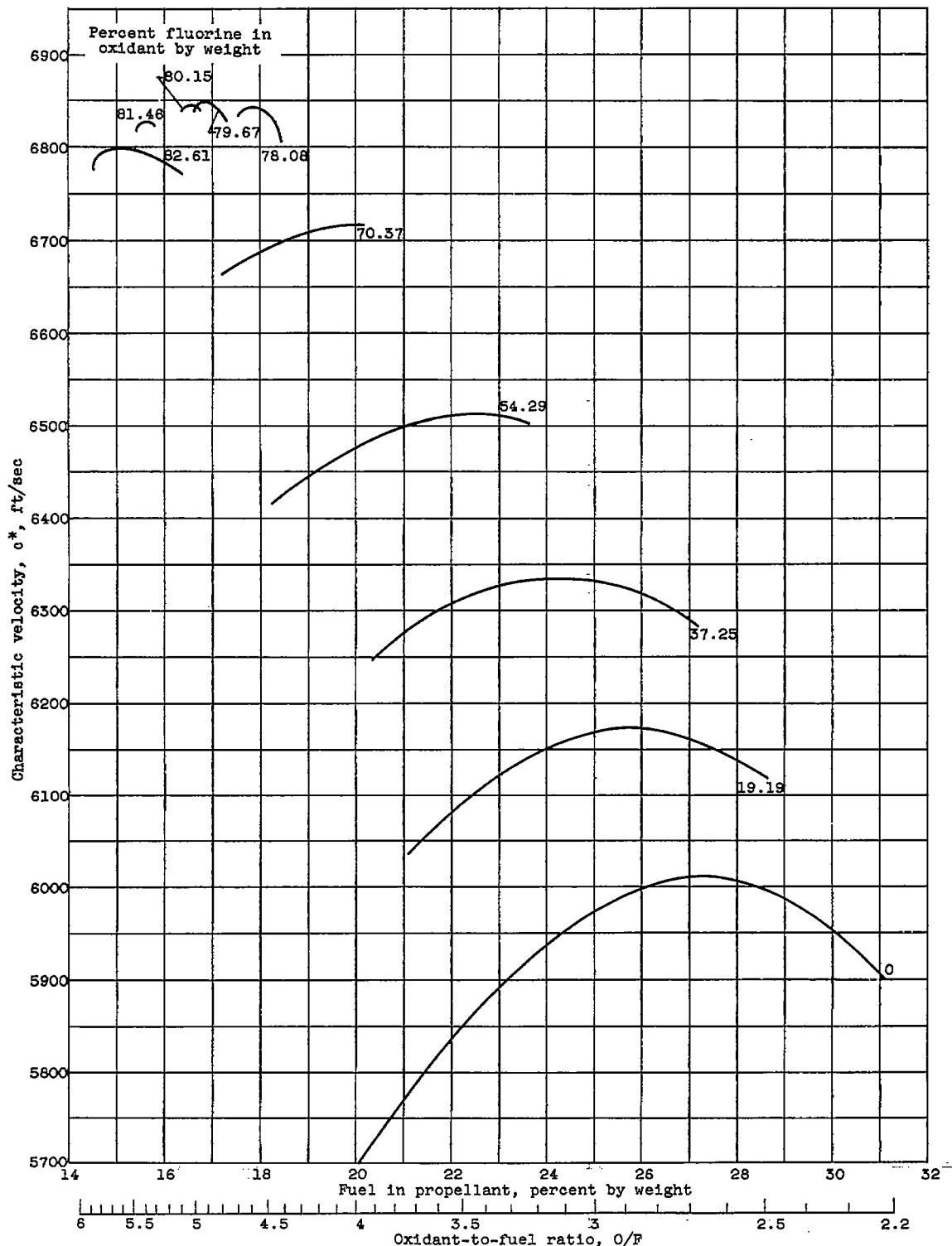


Figure 5. - Theoretical characteristic velocity for liquid methane with several fluorine-oxygen mixtures. Isentropic expansion assuming frozen composition from combustion-chamber pressure of 600 pounds per square inch absolute.

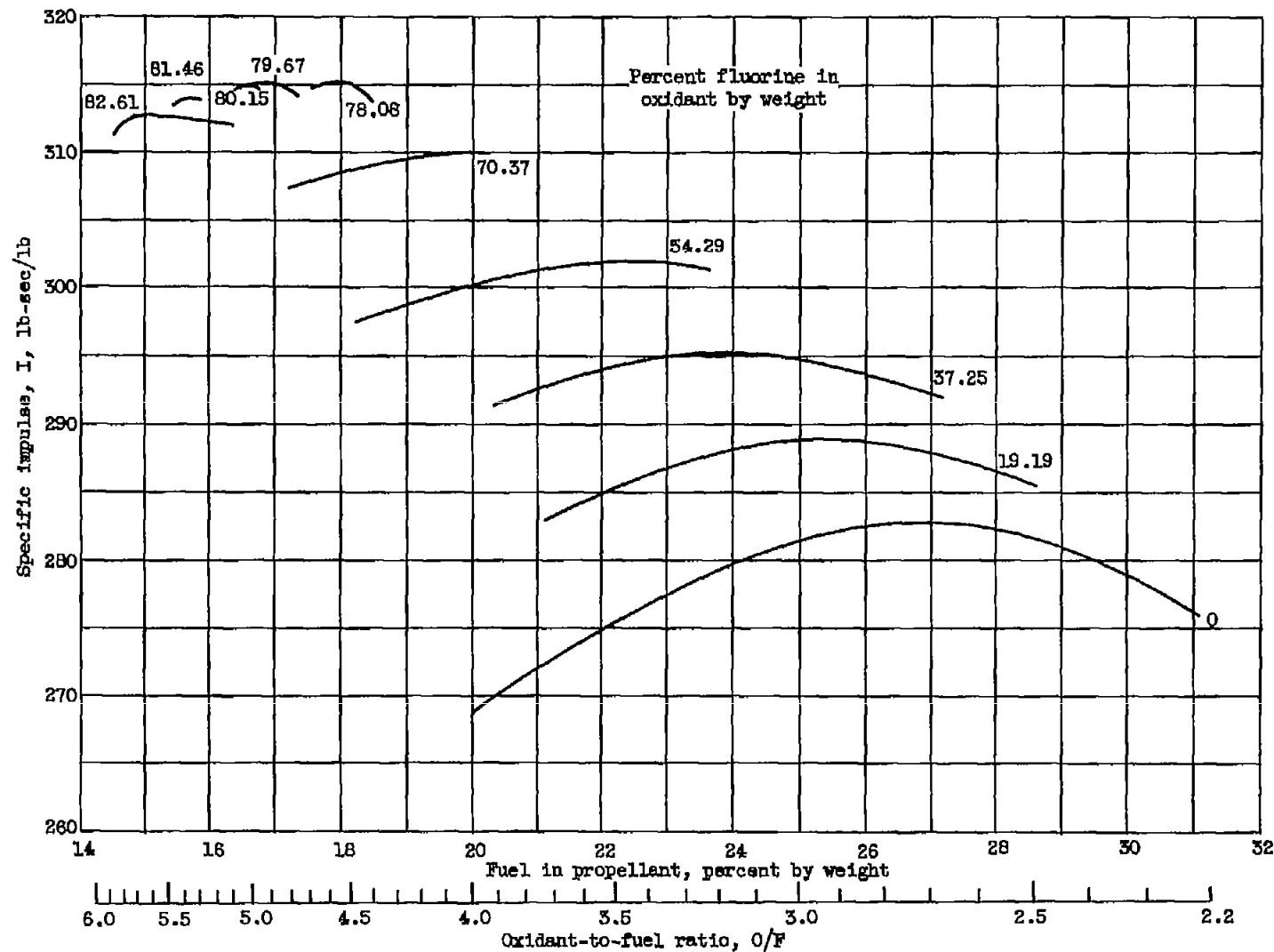


Figure 6. - Theoretical specific impulse for liquid methane with several fluorine-oxygen mixtures. Isentropic expansion assuming frozen composition from combustion-chamber pressure of 600 pounds per square inch absolute to exit pressure of 1 atmosphere.

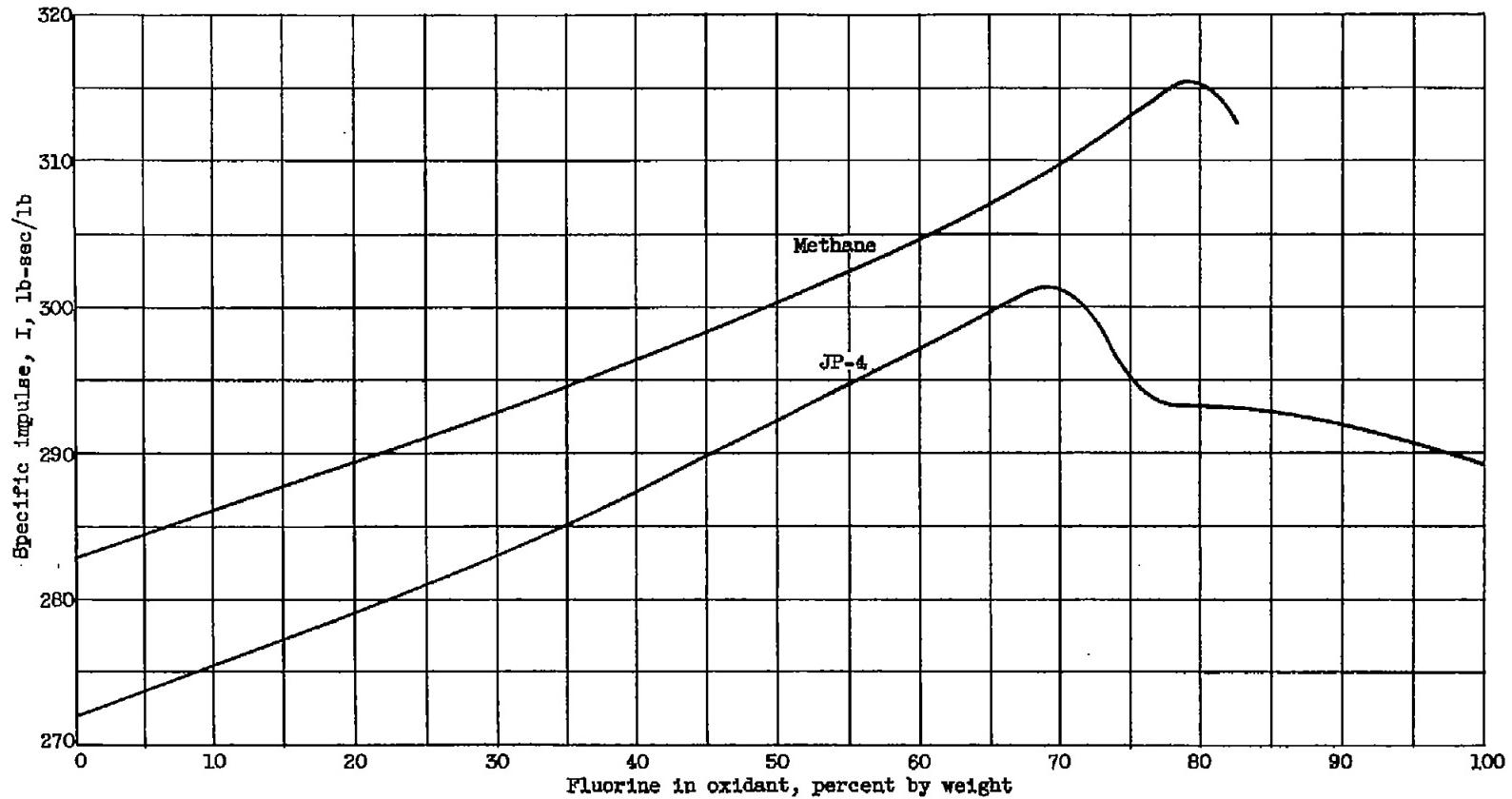


Figure 7. - Comparison of theoretical specific impulse of liquid methane with that of JP-4 fuel both with fluorine-oxygen mixtures at equivalence ratios for which specific impulse is maximum. Frozen composition assumed during isentropic expansion from combustion-chamber pressure of 600 pounds per square inch absolute to 1 atmosphere.